

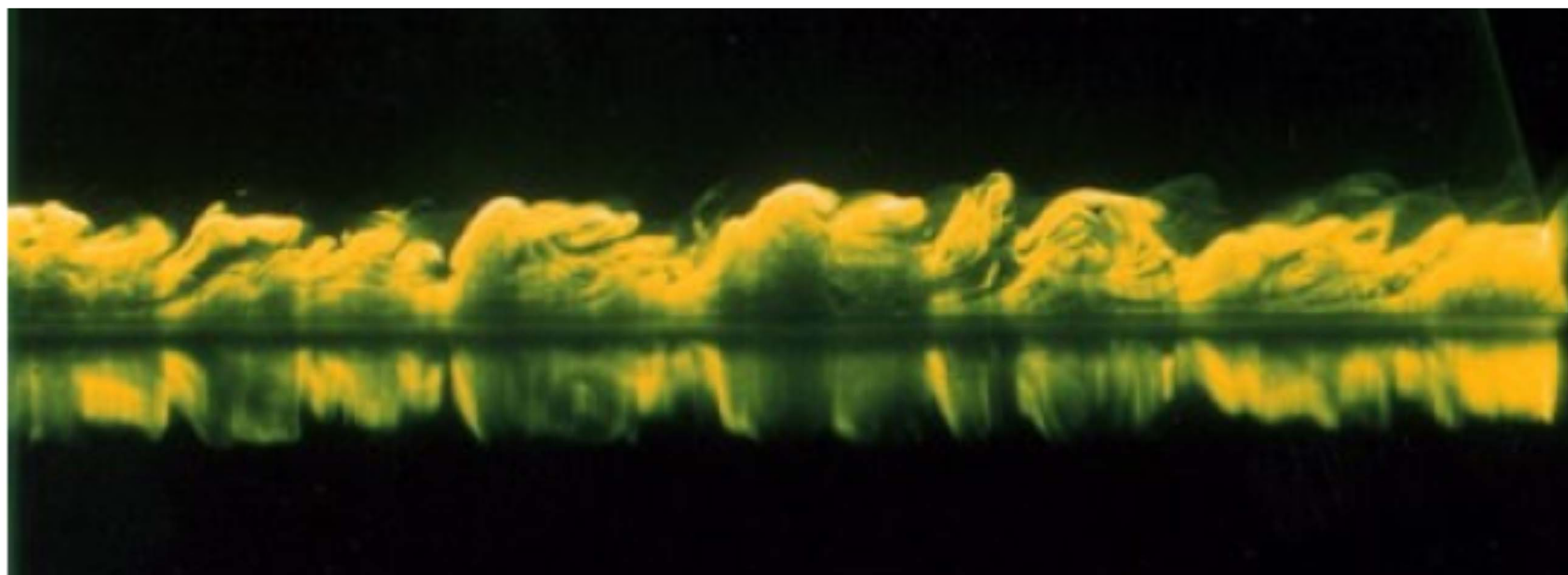


Turbulence

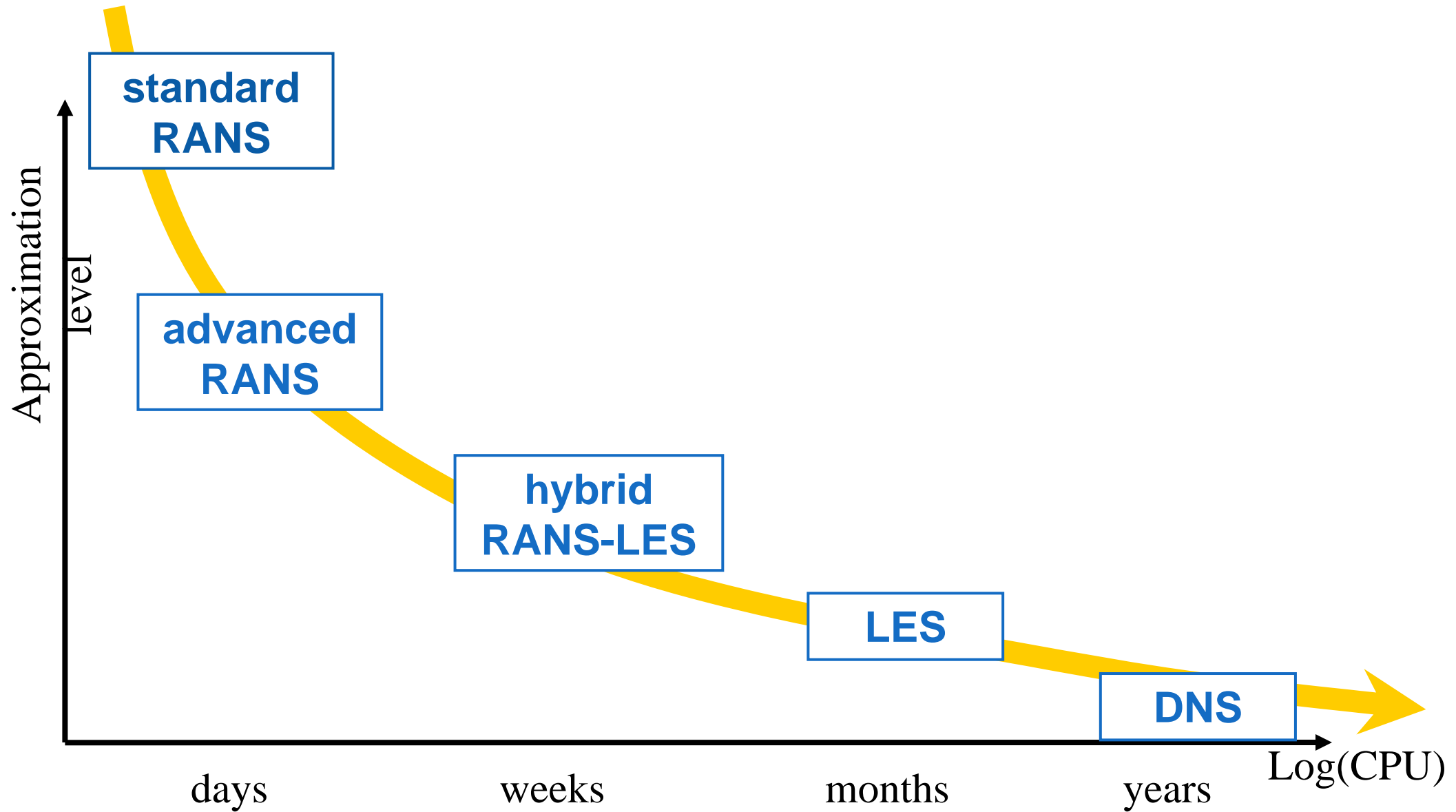
There are no “simple” turbulent flows

Turbulent boundary layer:

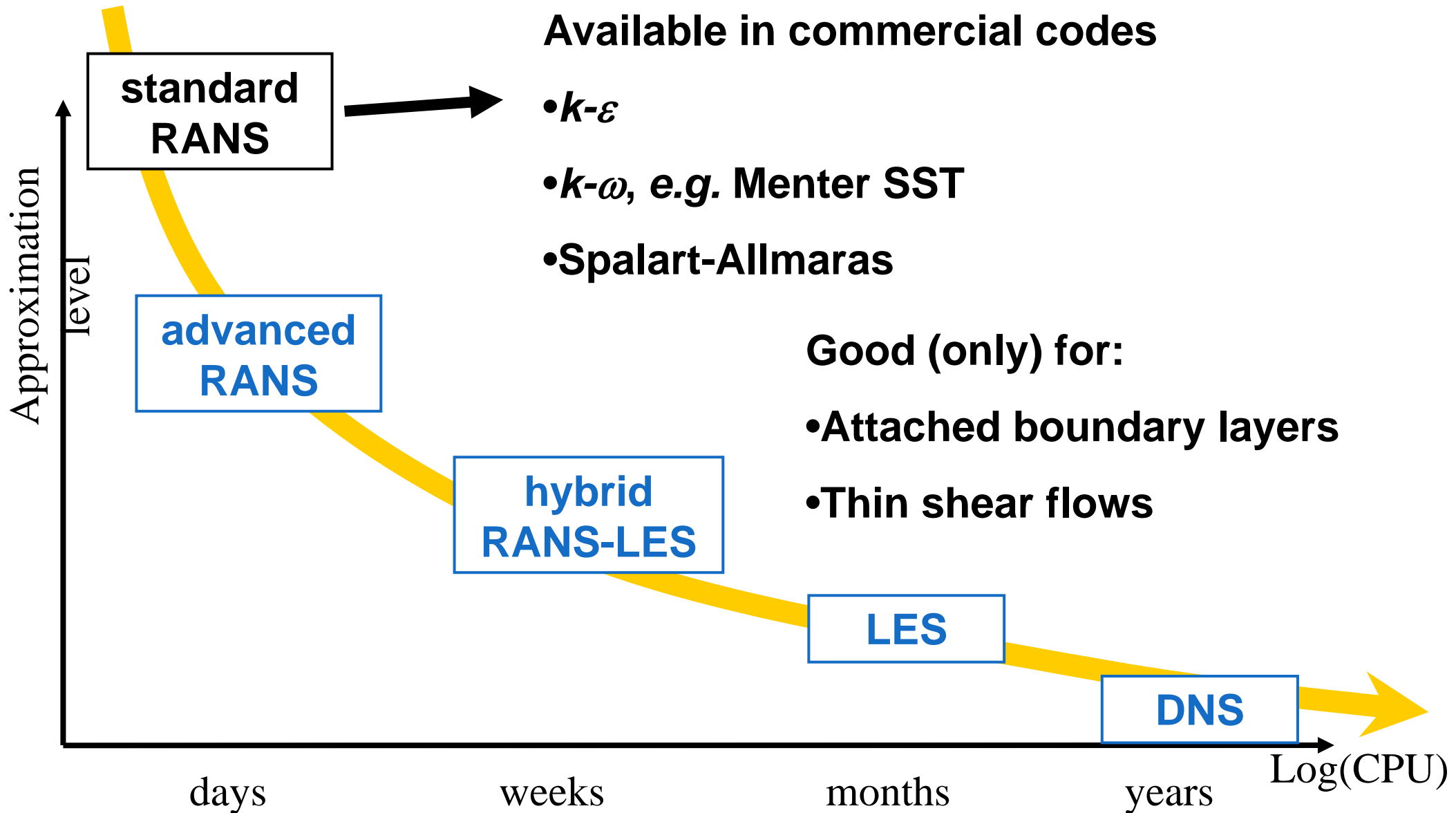
- Instantaneous velocity field (snapshot) $u_i(\mathbf{x}, t)$



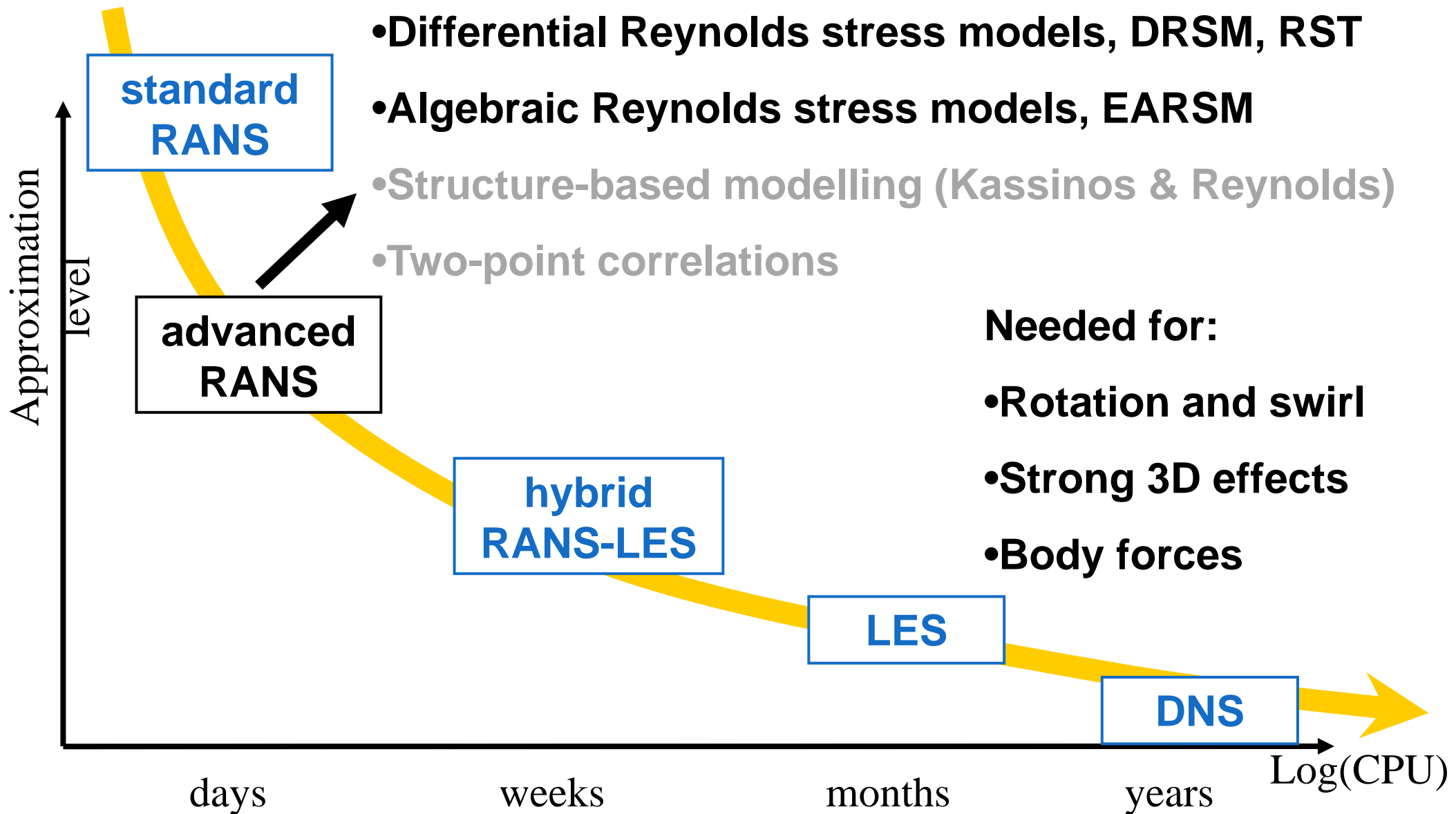
Prediction of turbulent flows



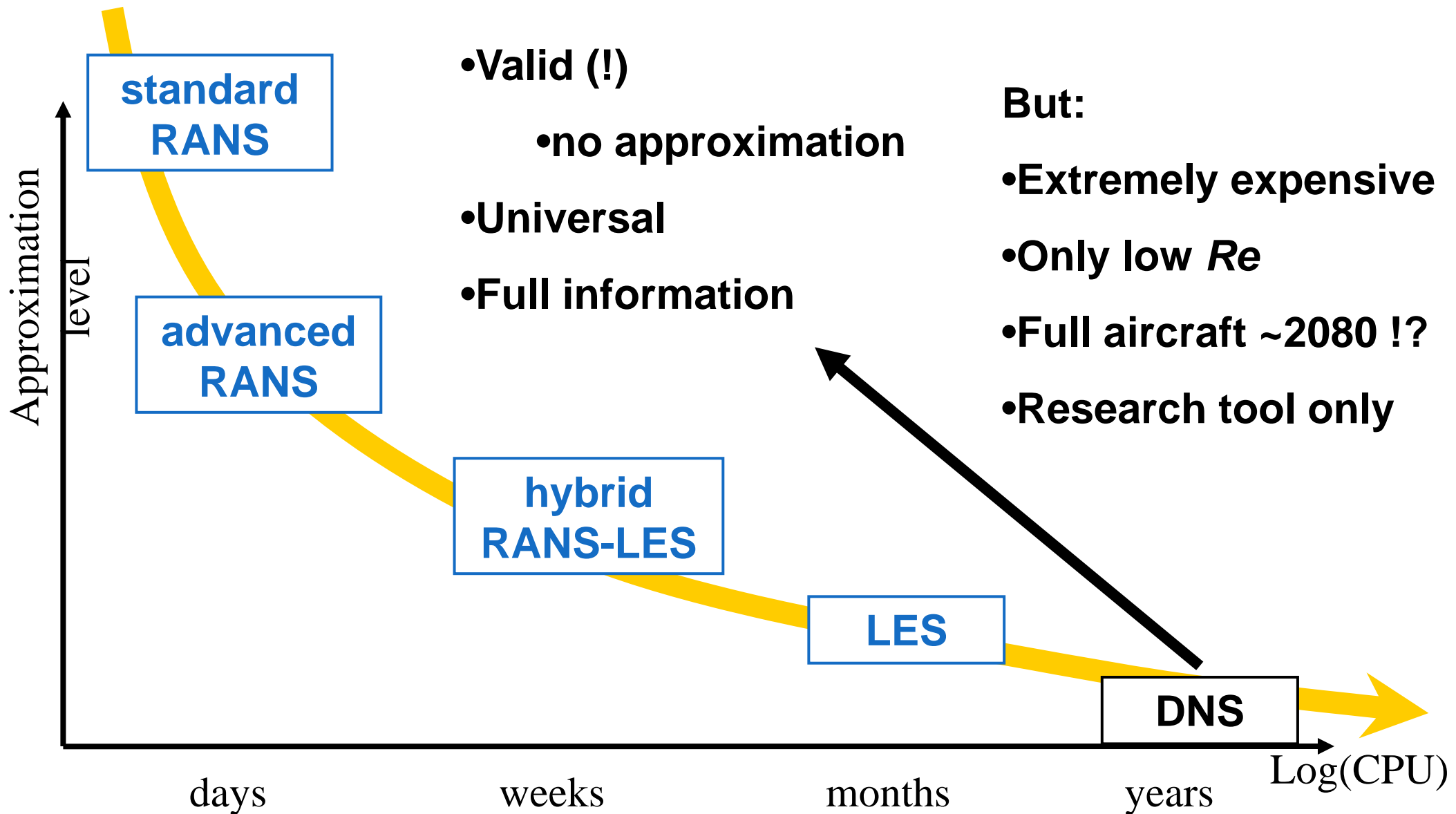
Standard RANS models



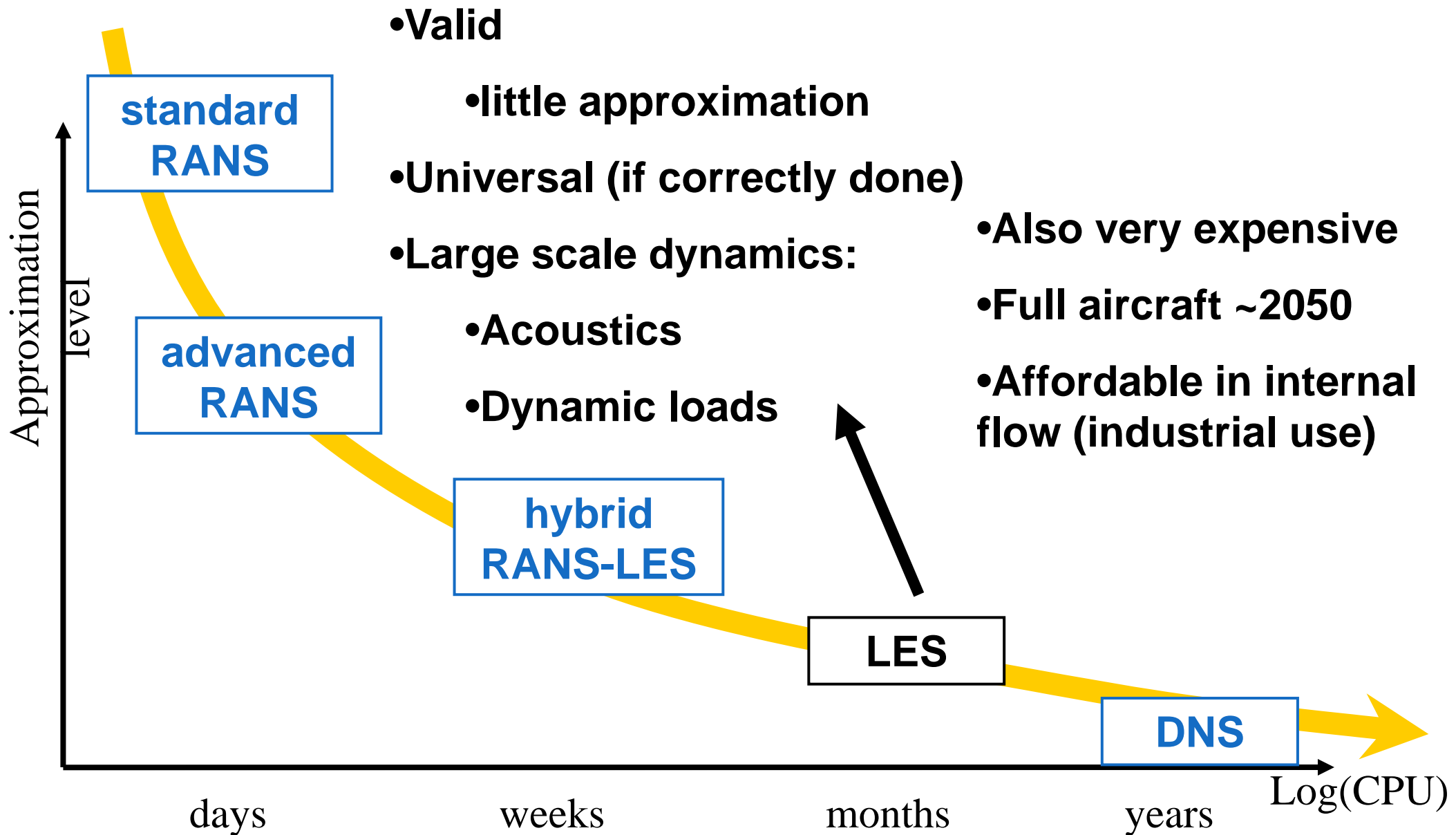
Advanced RANS models



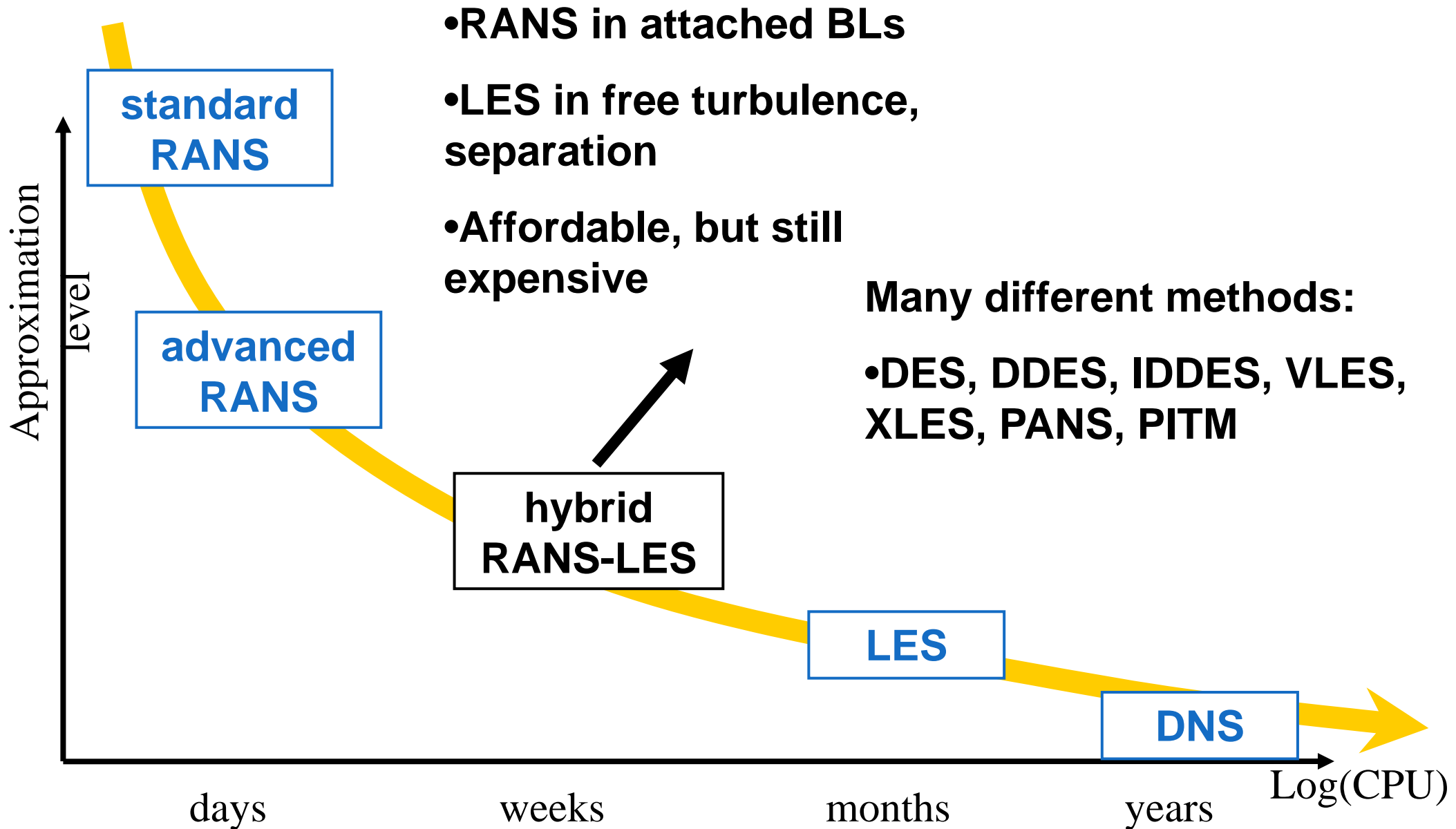
Direct Numerical Simulation – DNS



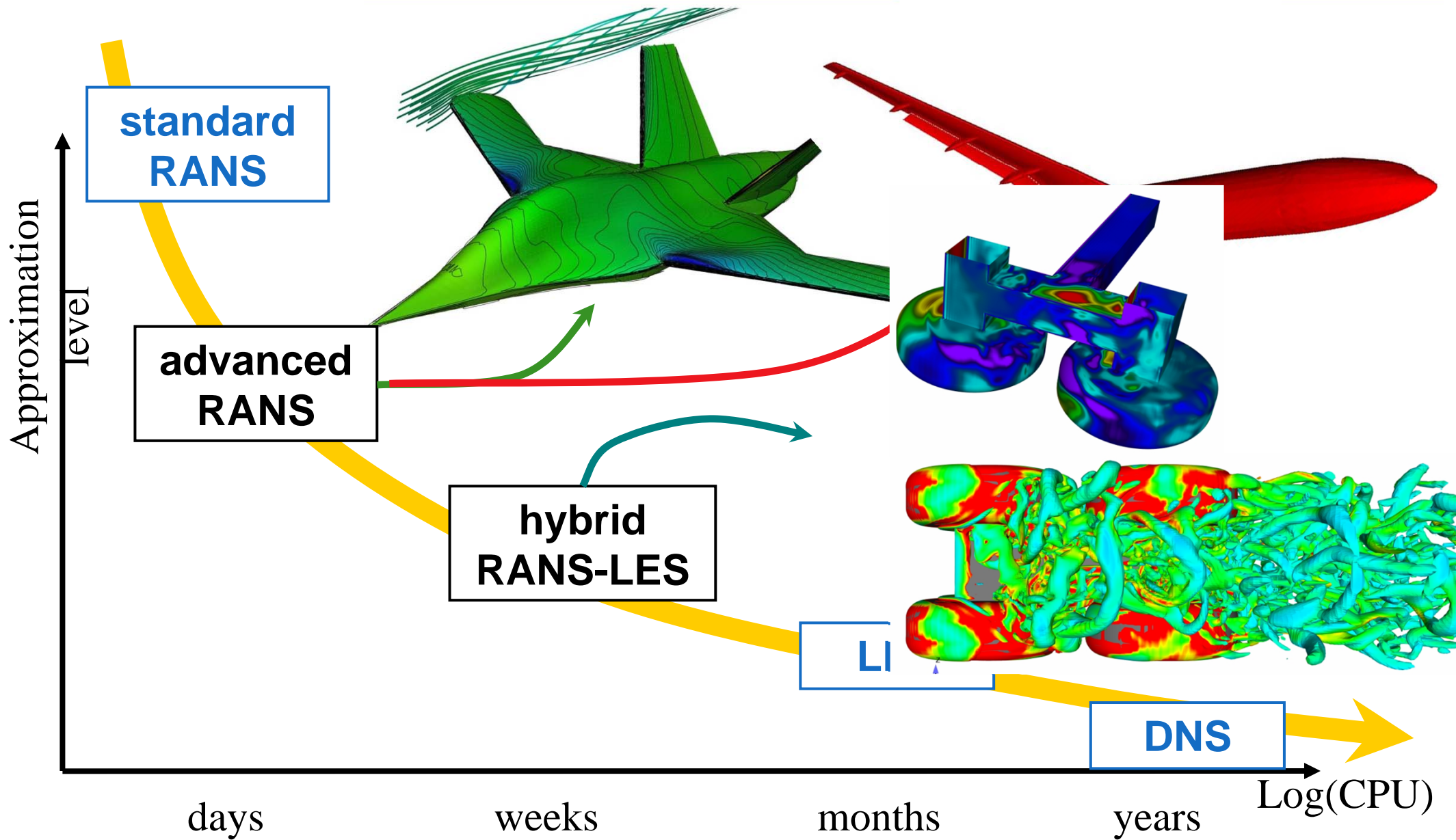
Large Eddy Simulation – LES



Hybrid RANS – LES methods



Prediction of turbulent flows



Basic concepts



- Turbulence is:
 - random fluctuations
 - 3D
 - time dependent
 - present in most flows of engineering interest
- Energy cascade
 - generated at the largest scales (L and U)
 - large scale vortices break down to smaller vortices
 - dissipates to heat at the smallest viscous scales, ε
 - balanced cascade

$$\varepsilon \sim \frac{U^3}{L}$$

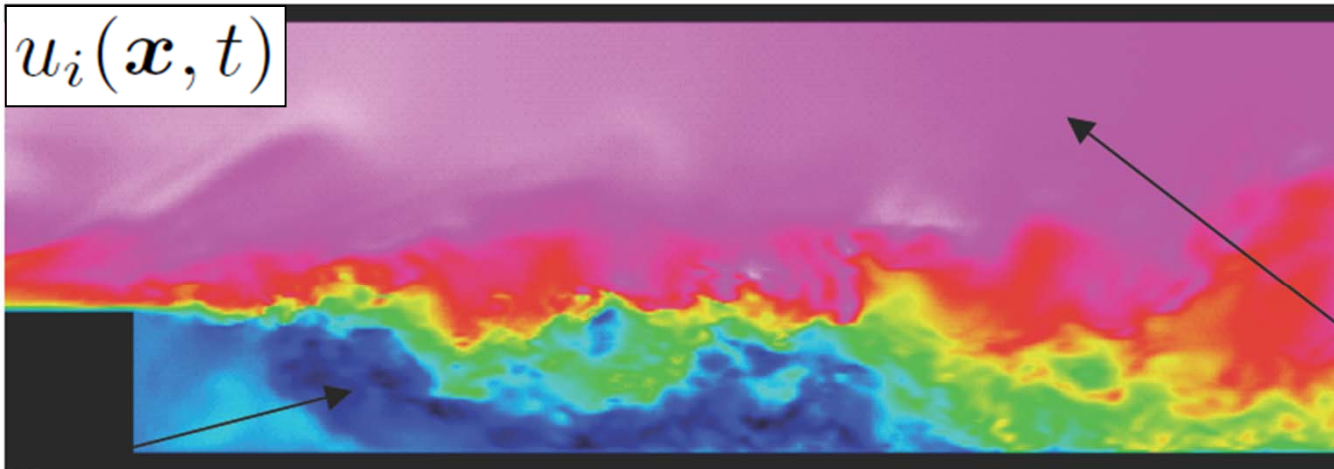
- turbulent kinetic energy

$$K \sim U^2$$

DNS/LES – RANS

DNS

Istantaneous

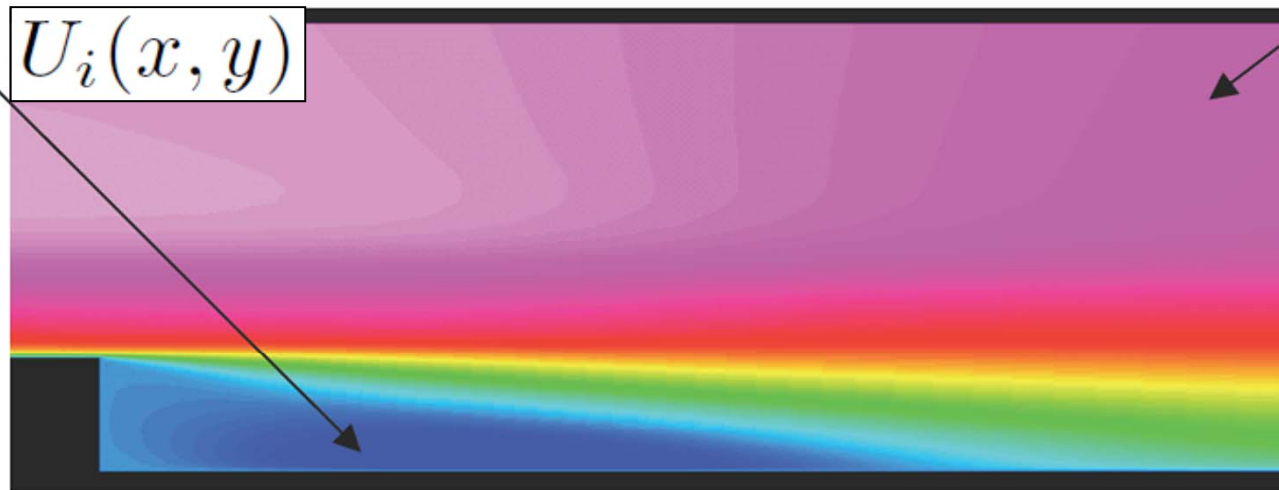


low velocity regions

high velocity regions

RANS

Time averaged

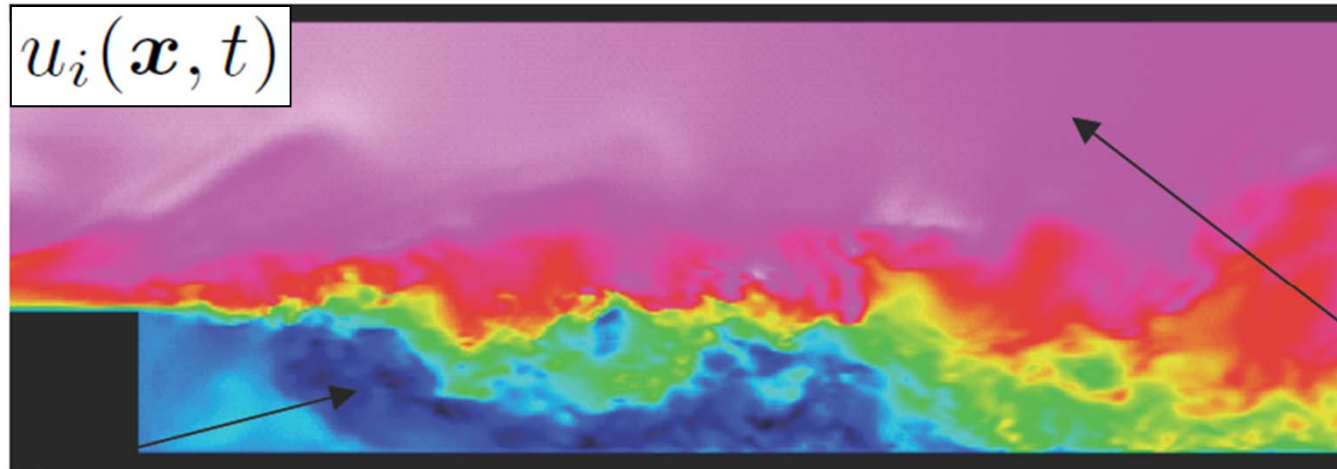


Length of the recirculation region is of engineering interest

DNS/LES – RANS

DNS

Istantaneous



low velocity
regions

high velocity
regions

DNS (and also LES):

- 3D
- Time dependent
 - Full information of turbulence scales
 - Acoustics and dynamic loads
 - No (limited) turbulence modelling
- Huge Reynolds number dependency

Expensive!

DNS/LES – RANS

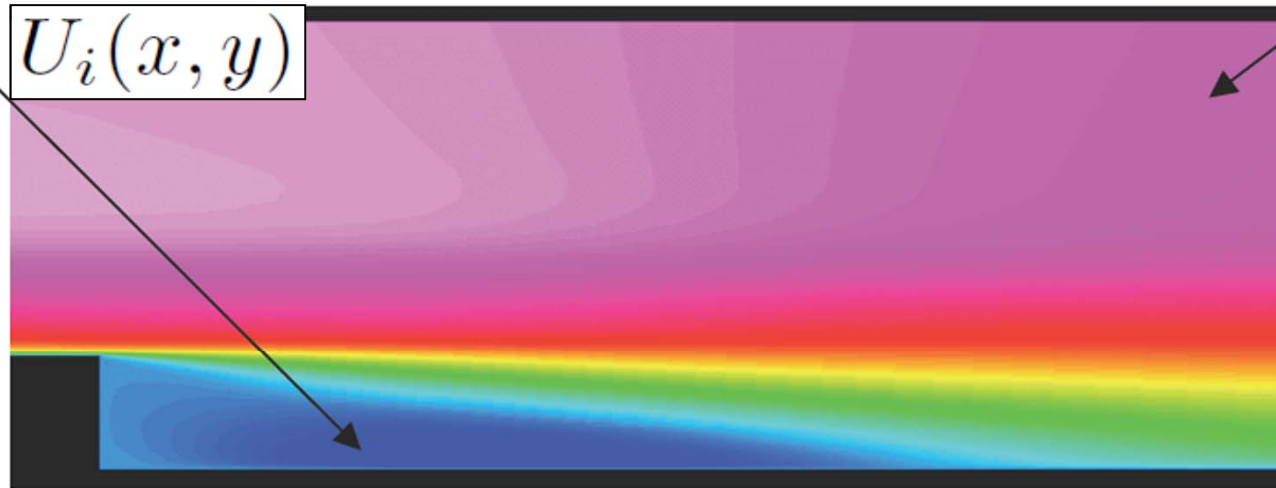
RANS:

- Reduction of dimensions → cheap
Here: 2D and steady
- Only statistical information of turbulence scales:
Time and length scales
rms values
- Turbulence model needed

low velocity
regions

RANS

Time averaged



Length of the recirculation region is of engineering interest

Scale separation



- Large scales L and U related to geometrical scales
- Small viscous scales (related to ν and ε)

$$l_K = \eta \sim \left(\frac{\nu^3}{\varepsilon}\right)^{1/4}, \quad t_K \sim \sqrt{\frac{\nu}{\varepsilon}}$$

- Scale separation

$$\frac{L}{\eta} \sim Re^{3/4}, \quad \frac{t}{t_K} \sim Re^{1/2}$$

- Reynolds number

$$Re = \frac{LU}{\nu}$$

Different Reynolds numbers



- Based on global scales

$$Re_L = \frac{LU}{\nu}$$

- Based on distance x from leading edge (flat plate)

$$Re_x = \frac{xU}{\nu}$$

- Based on boundary layer thickness (δ)

$$Re_\delta = \frac{\delta U}{\nu}$$

- Based on wall skin friction

$$Re_\tau = \frac{\delta u_\tau}{\nu}$$

Viscosity

- Kinematic viscosity, ν
- Dynamic viscosity, μ
- Density, ρ

$$\mu = \rho\nu$$

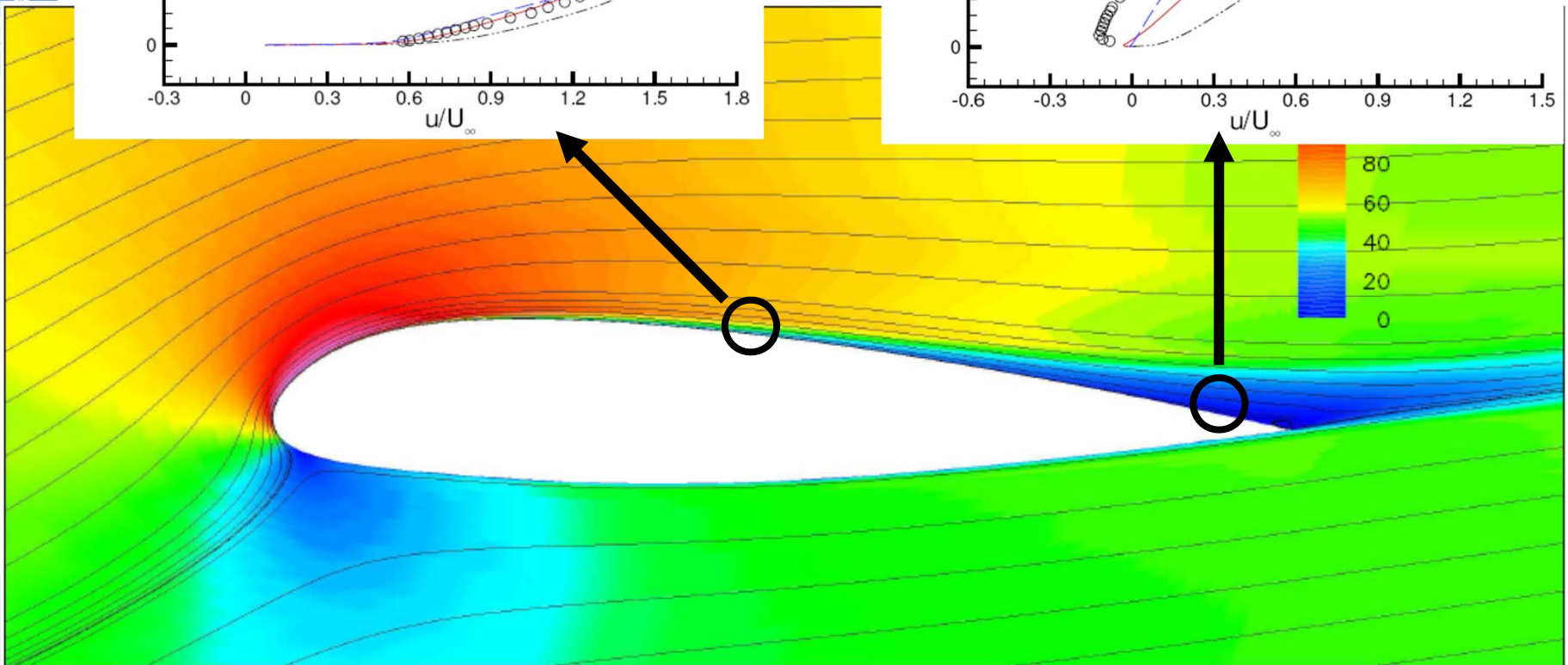
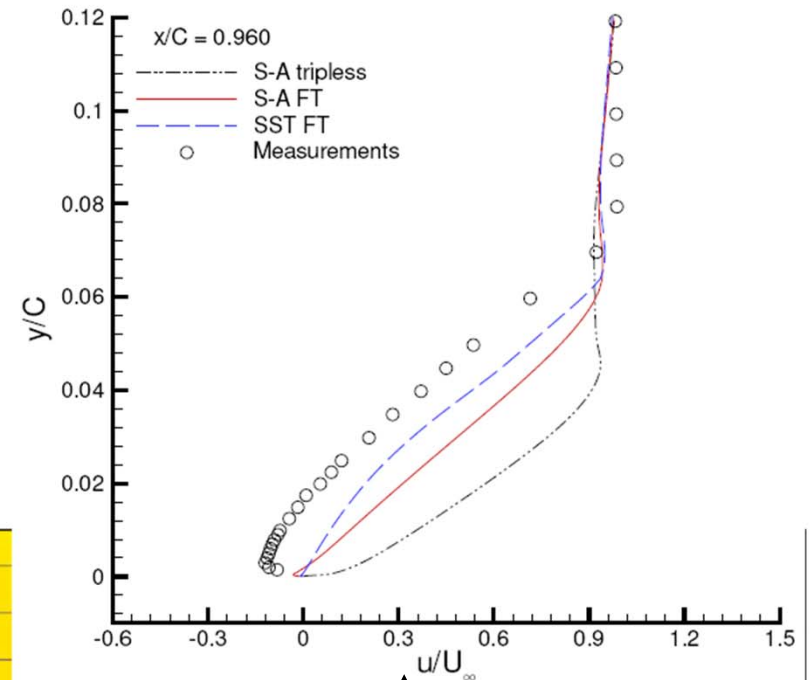
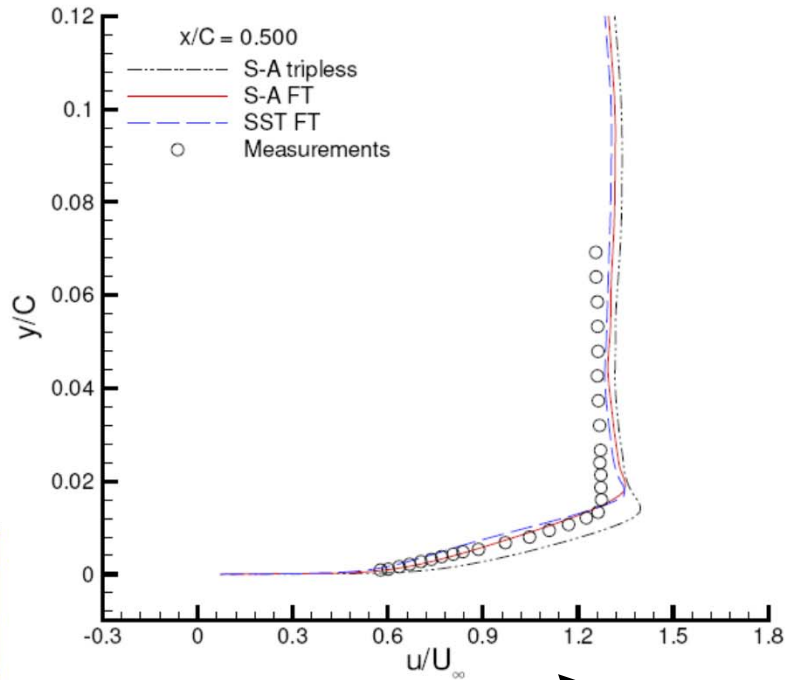


Boundary layers (BL)

- Thin layers
 - Thickness Reynolds number dependent
- Laminar boundary layers
 - Thickness related to wall skin friction
- Turbulent boundary layers
 - Inner and outer scales separated
 - Scale separation Reynolds number dependent



BL on the ONERA A-profile



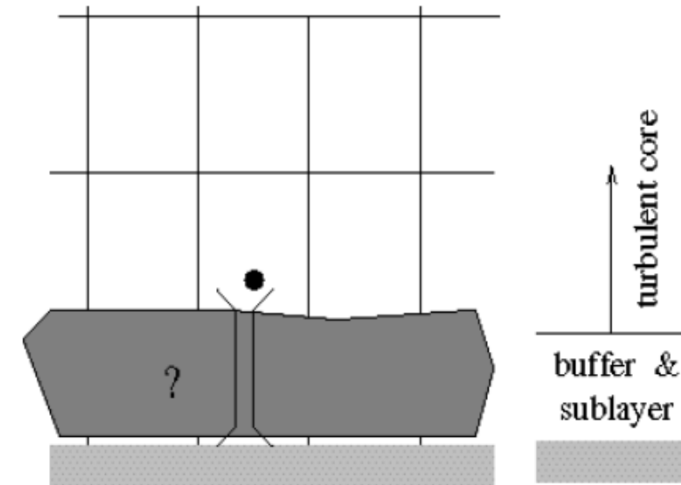
Approximation of BLs



- Slip wall boundary condition
 - Boundary layer completely neglected
 - Euler (non-viscous) computations possible
 - Slip BC can also be applied to viscous & turbulent CFD
- No slip boundary condition
 - Boundary layer completely resolved ($y^+ = 1$)
 - Extreme resolution needed ($\Delta y = 1-100\mu\text{m}$)
 - 40-80 grid points within the boundary layer
- Log-law boundary condition (turbulence)
 - First grid point within log layer ($y^+ > 20$ AND $y < 0.1\delta$)
 - 10-20 grid points within the boundary layer
 - Warning: standard log-law BCs inconsistent with too small grid size. READ SOLVER DOCUMENTATION !!!

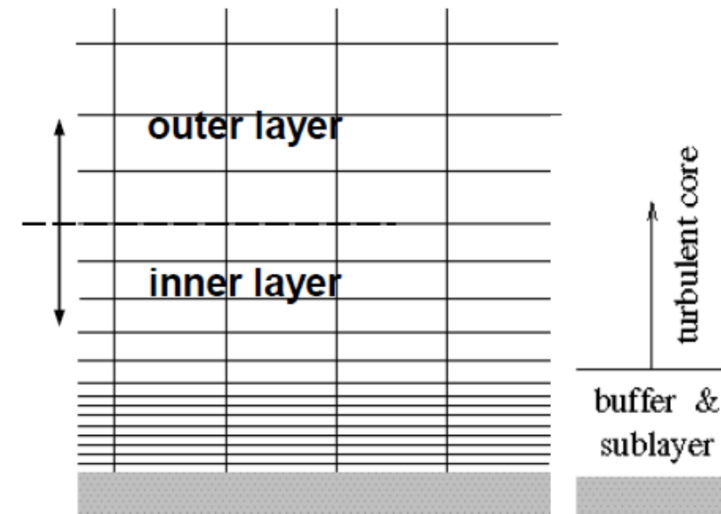
What's in Fluent?

- Standard and Non-Equilibrium Wall Functions:
 - “Wall adjacent cells should have y^+ values between 30 and 300–500” – (remember $y < 0.1\delta!$)
 - “The mesh expansion ratio should be small (no larger than around 1.2)”
 - “Non-equilibrium wall function method attempts to improve the results for flows with higher pressure gradients, separations, reattachment and stagnation”
- Scalable Wall Functions:
 - Consistent for all y^+ values



What's in Fluent? ...

- Enhanced Wall Treatment Option
 - Combines a blended law-of-the wall and a two-layer zonal model.
 - Suitable for low-Re flows or flows with complex near-wall phenomena.
 - Generally requires a fine near-wall mesh capable of resolving the viscous sublayer
 - $y^+ < 5$, and a minimum of 10–15 cells across the “inner layer” for best results
 - Valid for all y^+
 - Available for all k-e and k-w models
 - Not yet for Spalart-Allmaras ($y^+ < 3$ OR $y^+ > 15$)



Recommendations for Fluent

- For K - ε models
 - use Enhanced Wall Treatment: EWT- ε
- If wall functions are favored with K - ε models
 - use scalable wall functions
- For K - ω models
 - use the default: EWT- ω



Wall bounded turbulence

- Viscous wall scales

$$l_* = \frac{\nu}{u_\tau}, \quad t_* = \frac{\nu}{u_\tau^2}$$

- Wall friction velocity

$$u_\tau = \sqrt{\frac{\tau_w}{\rho}} = \sqrt{\nu \left. \frac{\partial U}{\partial y} \right|_{\text{wall}}} = U \sqrt{\frac{1}{2} C_f}$$

- Friction coefficient

$$C_f = \frac{\tau_w}{\frac{1}{2} \rho U^2} = 2 \left(\frac{u_\tau}{U} \right)^2$$

- Viscous wall distance

$$y^+ = \frac{y}{l_*} = \frac{y u_\tau}{\nu}$$



Empirical relations for BLs



- Friction coefficient

- Turbulent $\frac{C_f}{2} \approx 0,0296 Re_x^{-1/5}$

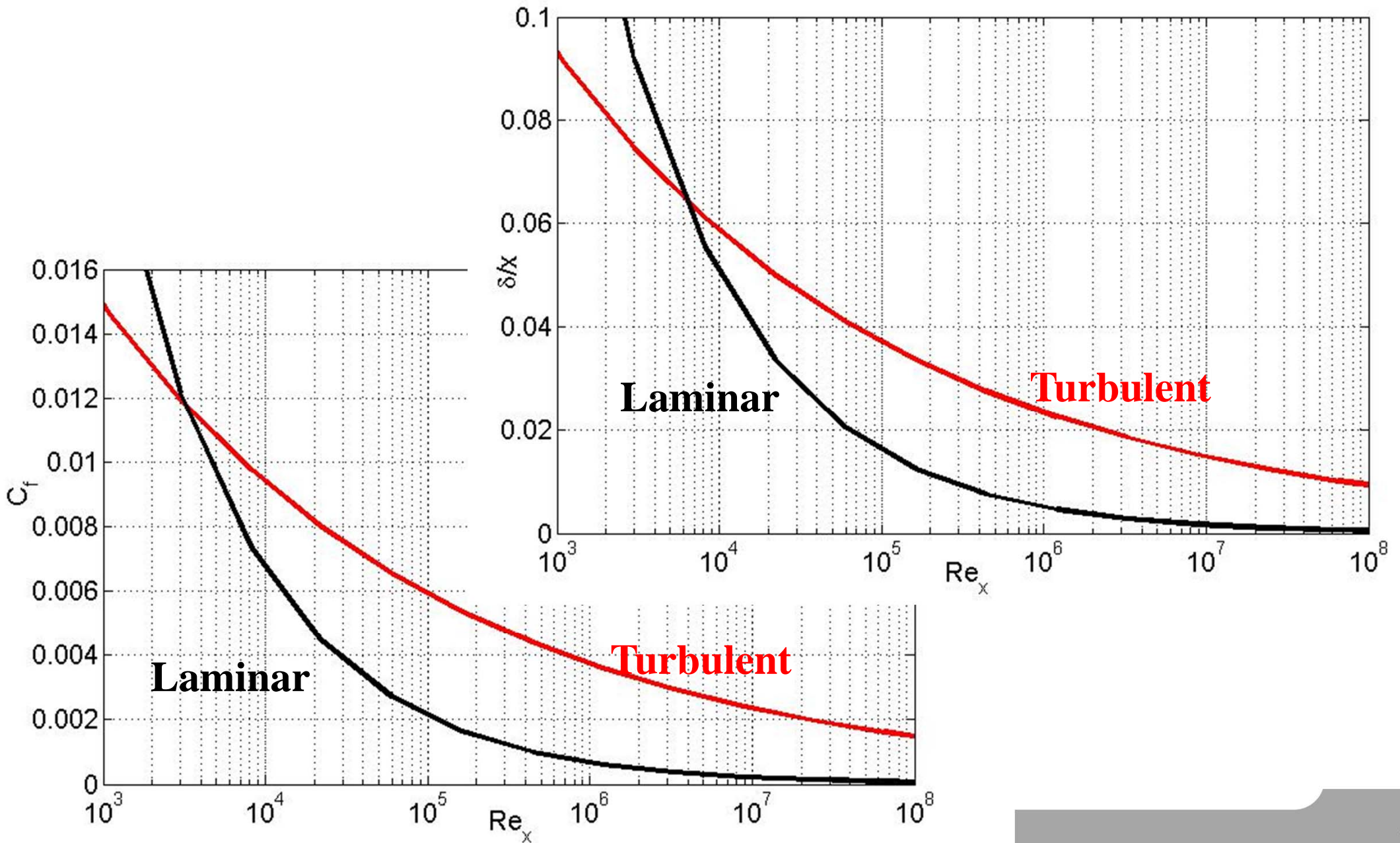
- Laminar $\frac{C_f}{2} = 0,332 Re_x^{-1/2}$

- Boundary layer thickness

- Turbulent $\frac{\delta}{x} \approx 0,37 Re_x^{-1/5}$

- Laminar $\frac{\delta}{x} = 5,0 Re_x^{-1/2}$

Empirical relations plotted



Empirical relations plotted

