

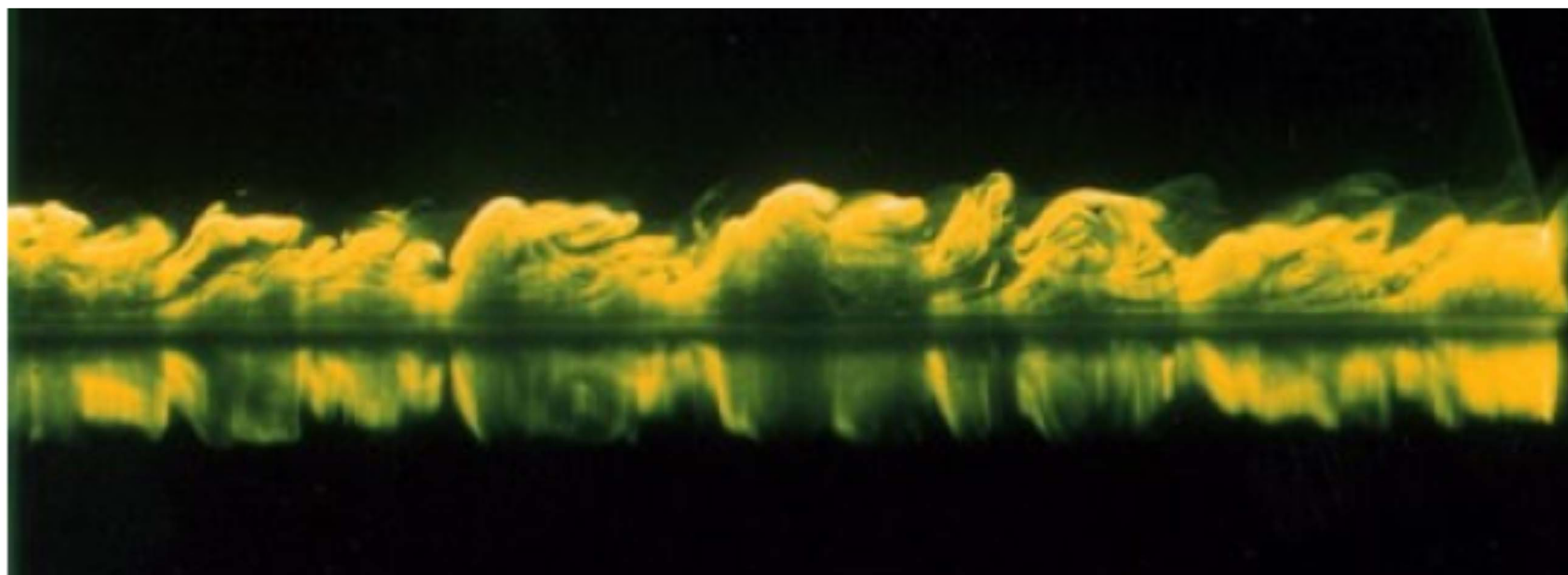


# Turbulence

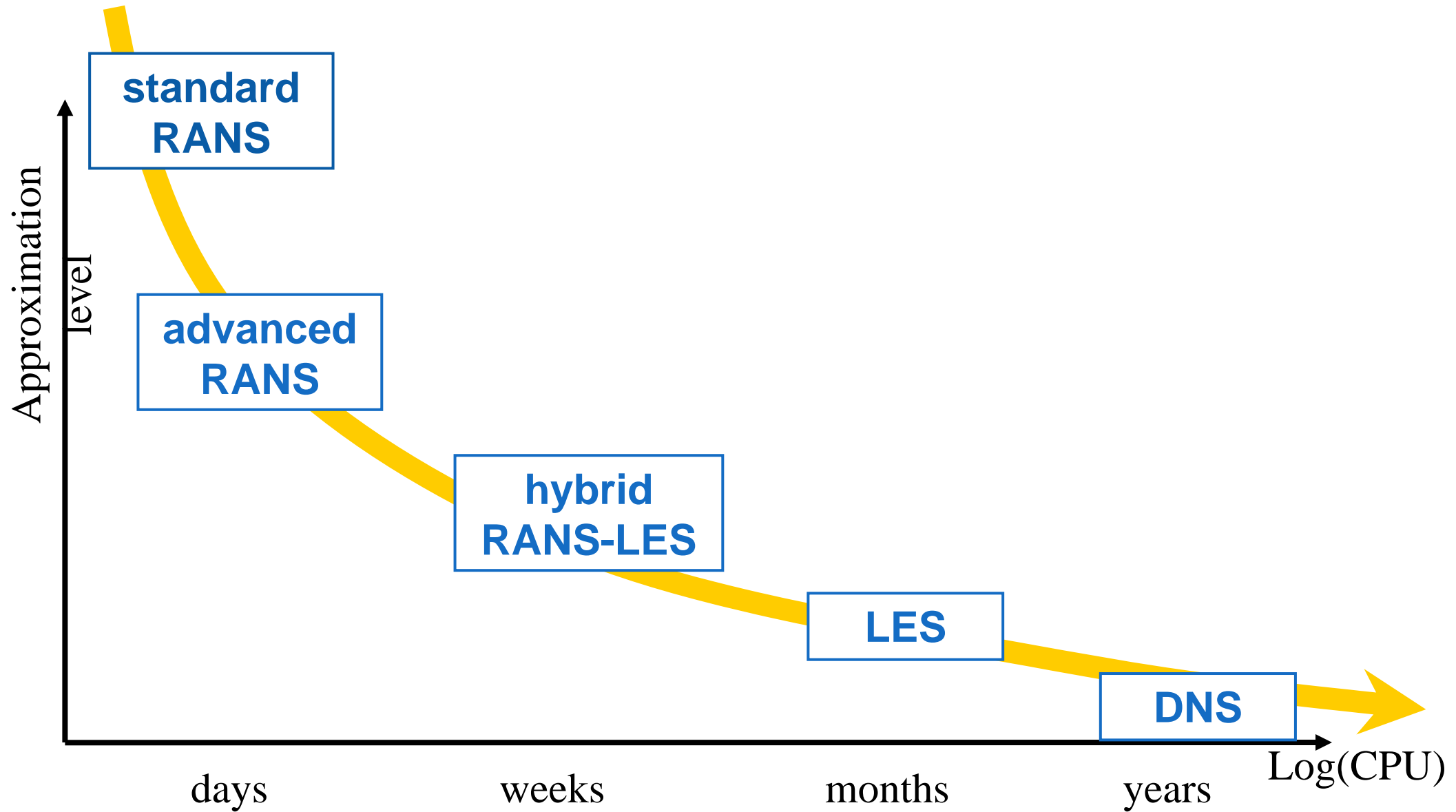
# There are no “simple” turbulent flows

Turbulent boundary layer:

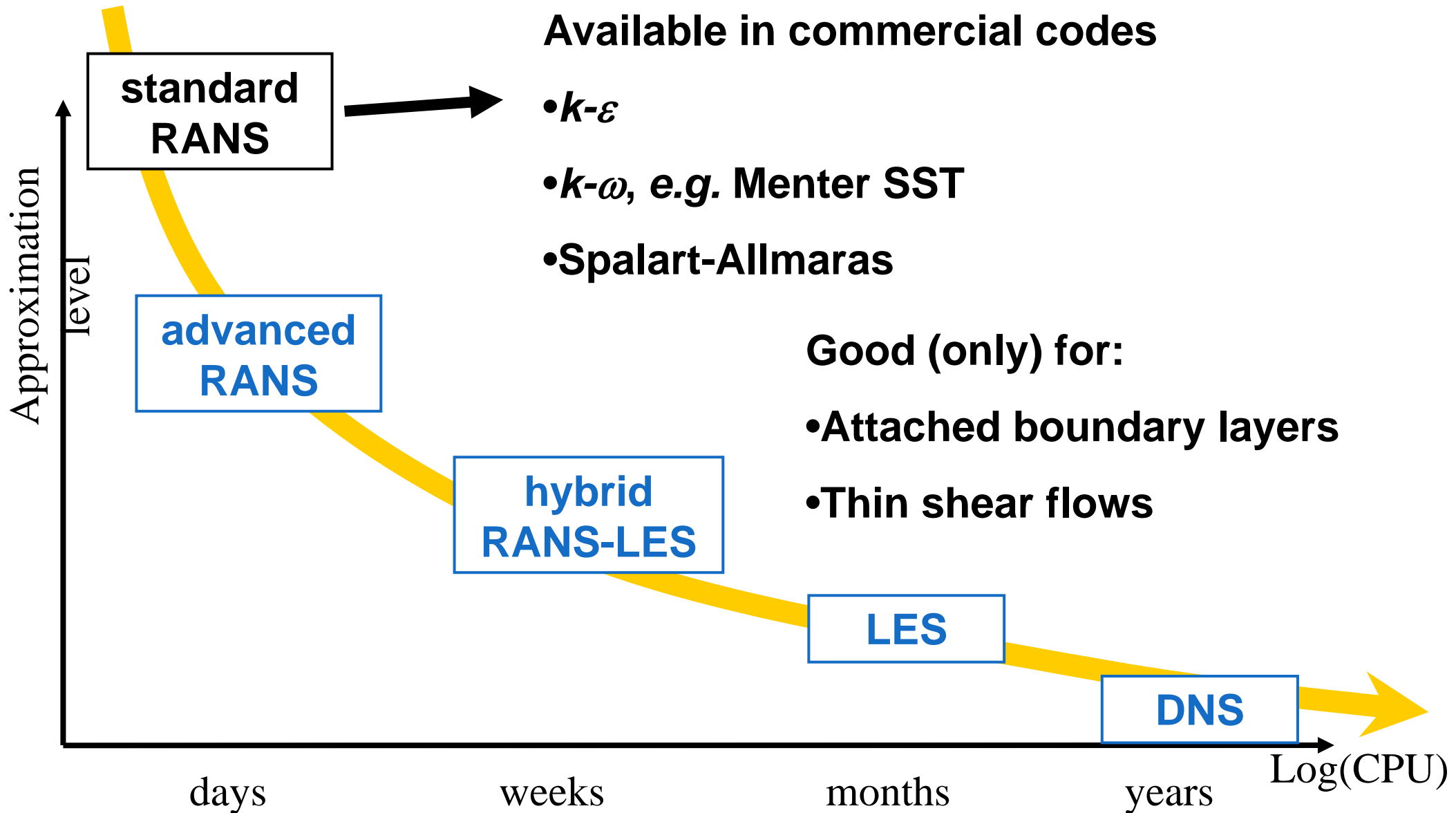
- Instantaneous velocity field (snapshot)  $u_i(\mathbf{x}, t)$



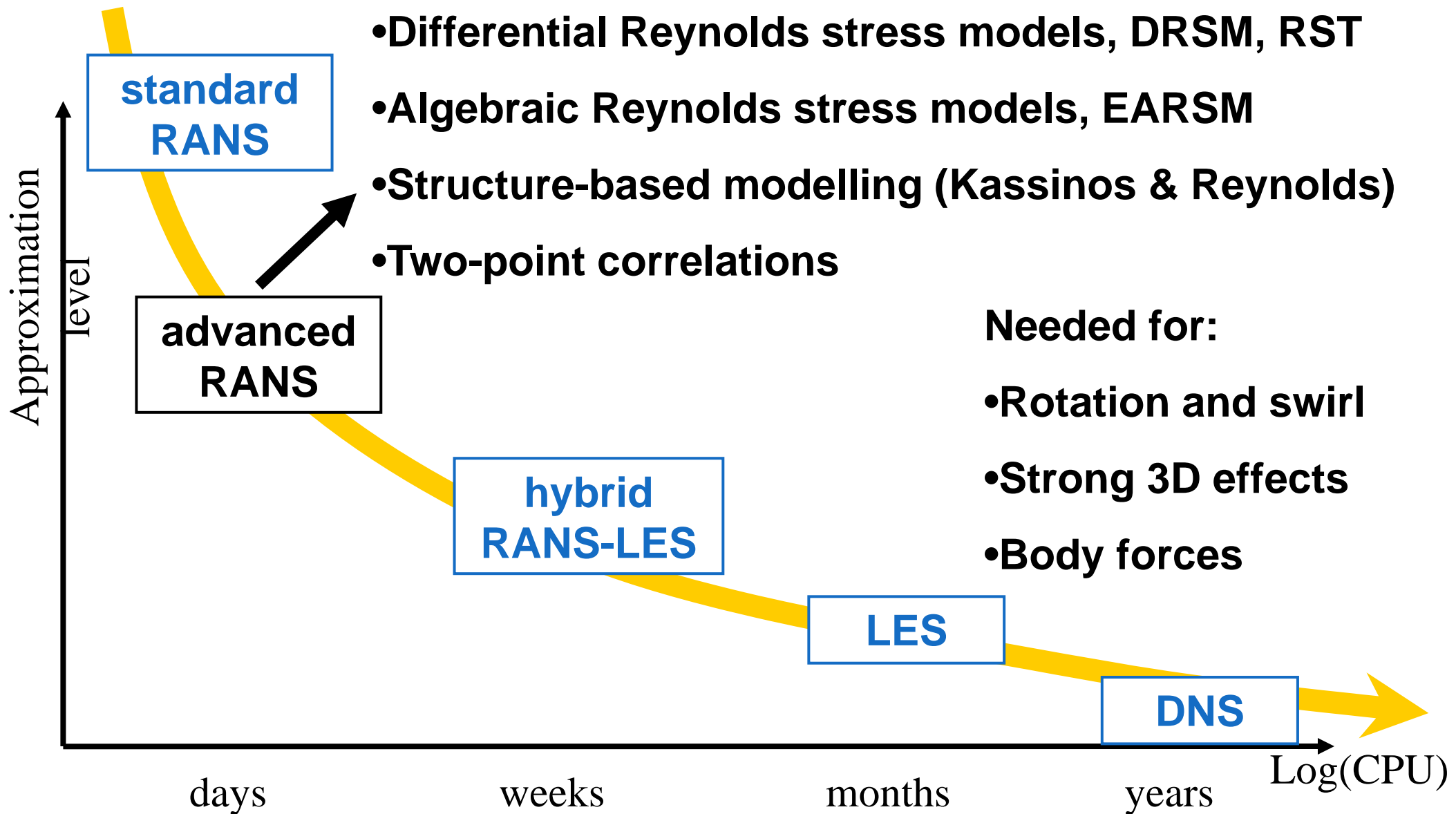
# Prediction of turbulent flows



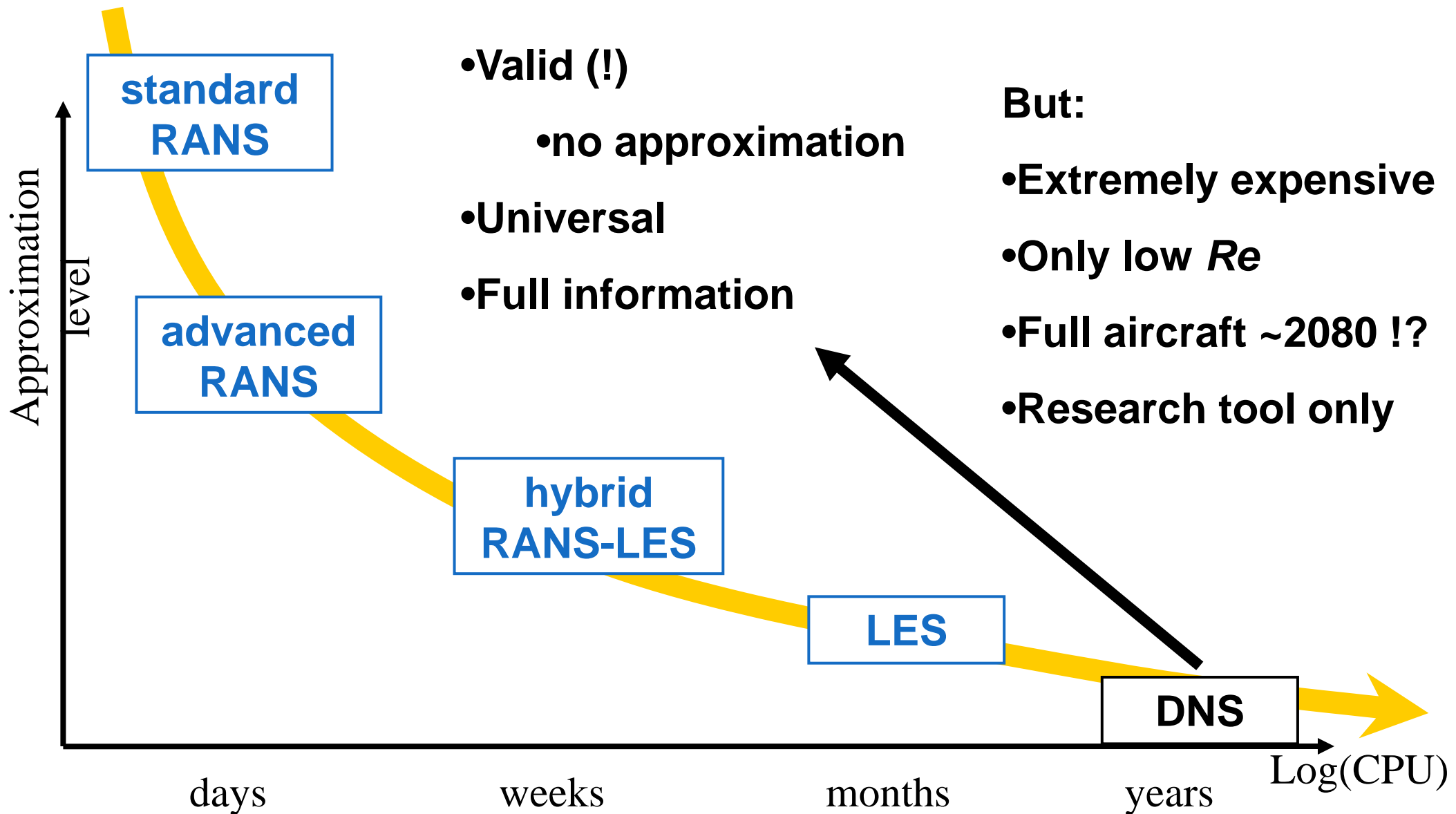
# Standard RANS models



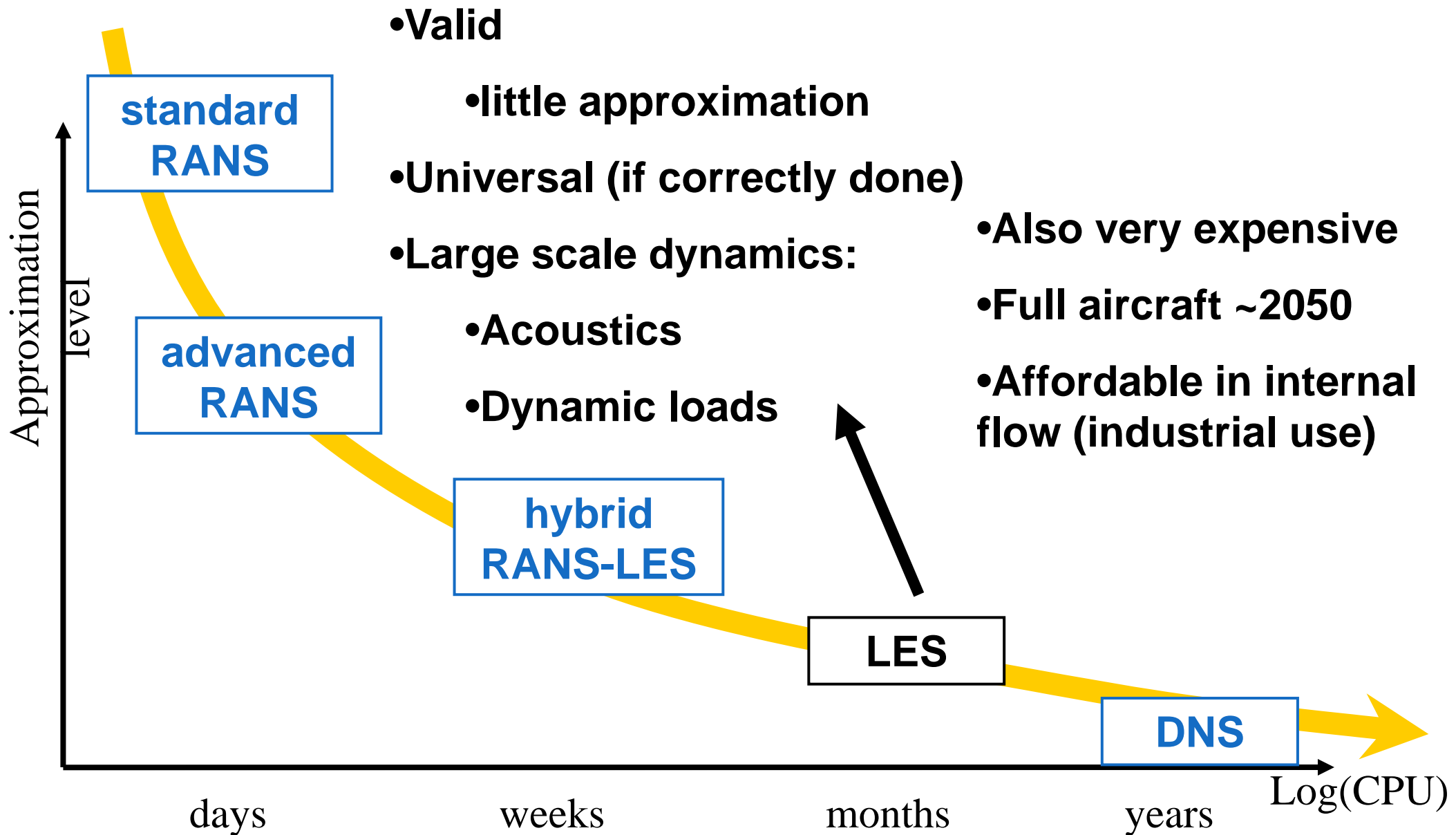
# Advanced RANS models



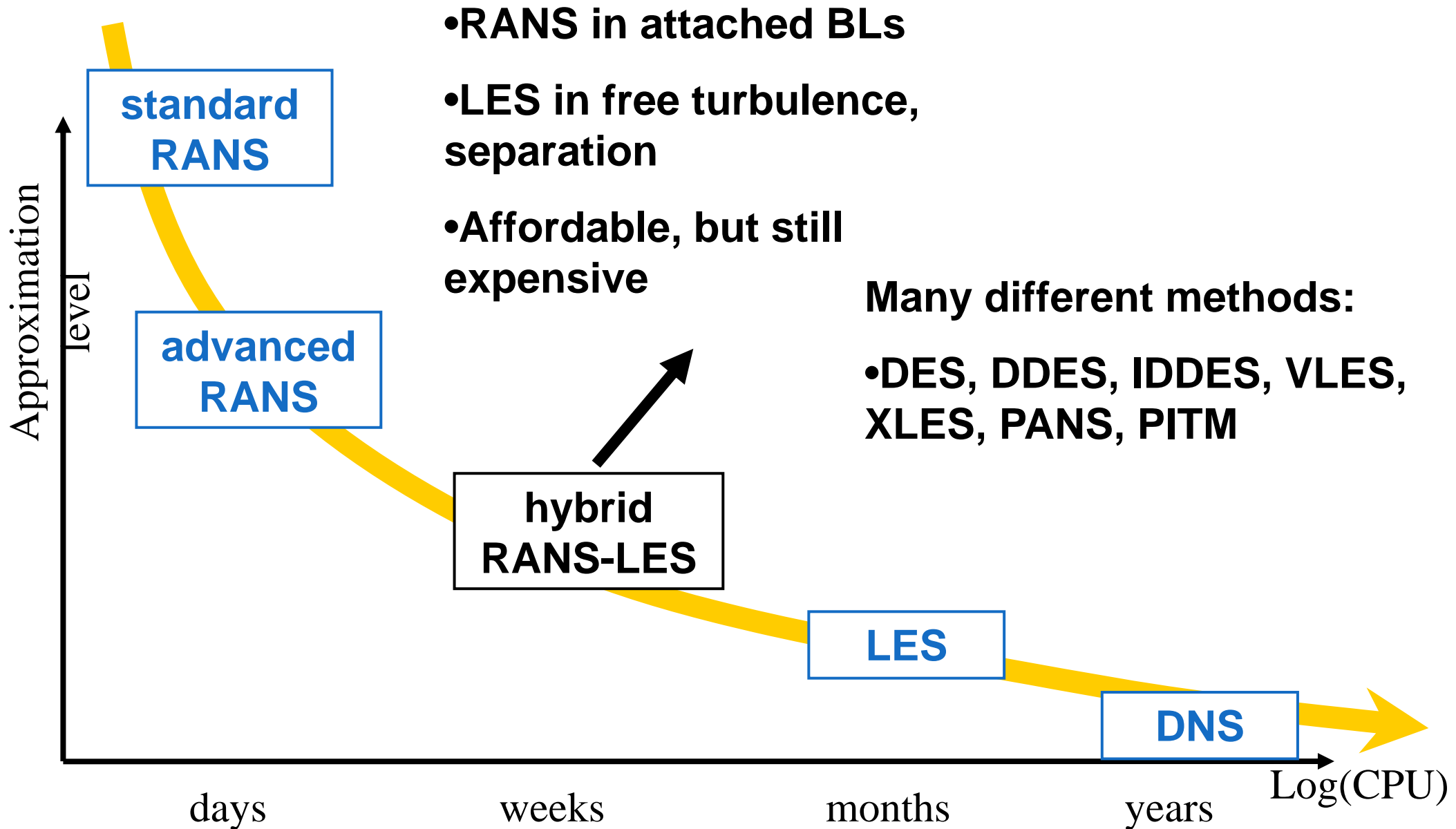
# Direct Numerical Simulation – DNS



# Large Eddy Simulation – LES

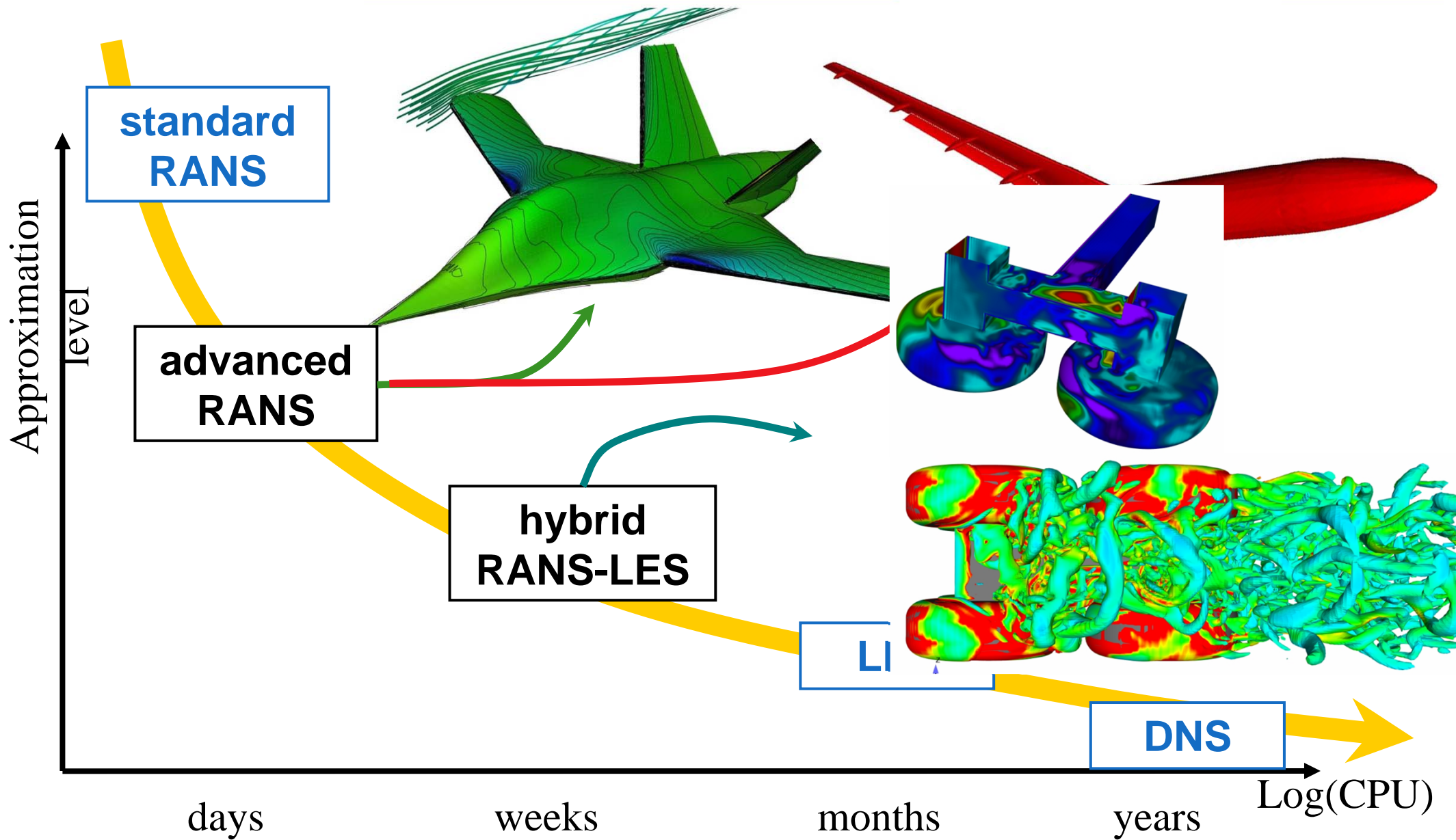


# Hybrid RANS – LES methods





# Prediction of turbulent flows



# Basic concepts



- Turbulence is:
  - random fluctuations
  - 3D
  - time dependent
  - present in most flows of engineering interest
- Energy cascade
  - generated at the largest scales ( $L$  and  $U$ )
  - large scale vortices break down to smaller vortices
  - dissipates to heat at the smallest viscous scales,  $\varepsilon$
  - balanced cascade

$$\varepsilon \sim \frac{U^3}{L}$$

- turbulent kinetic energy

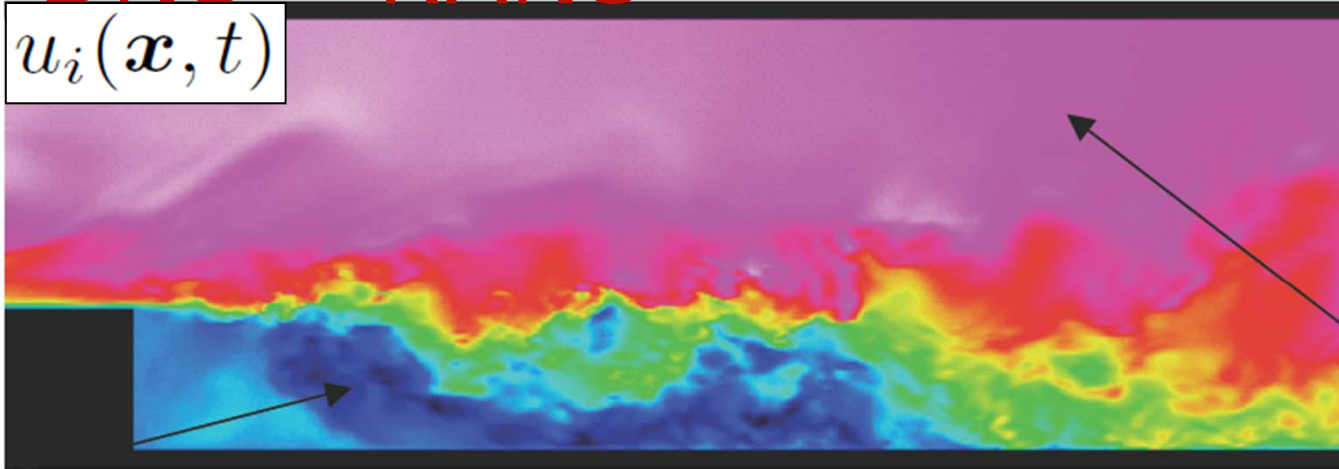
$$K \sim U^2$$

# DNS – RANS

**DNS**

Istantaneous

$$u_i(\mathbf{x}, t)$$



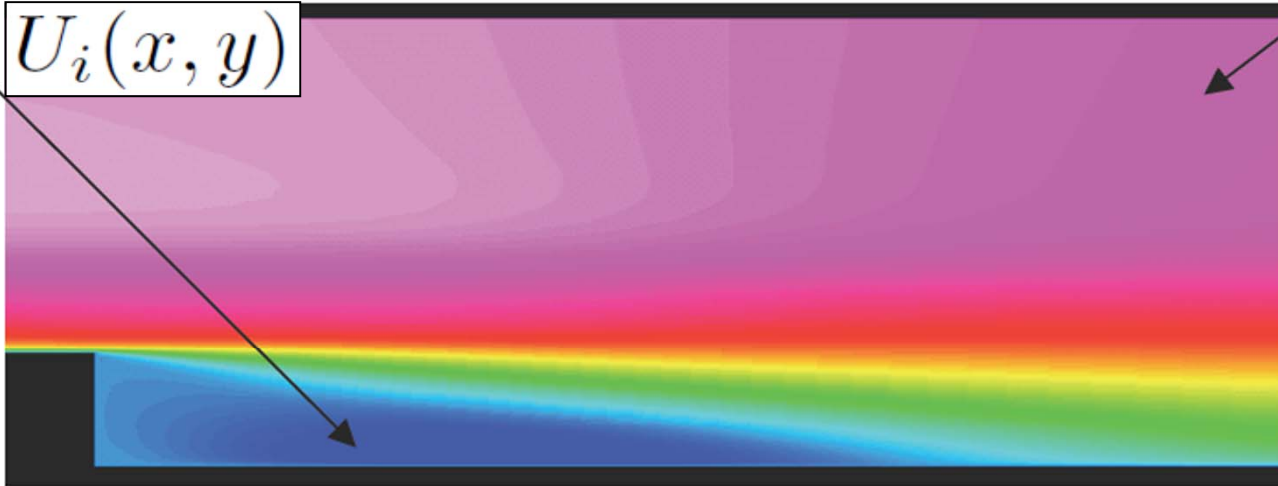
low velocity regions

high velocity regions

**RANS**

Time averaged

$$U_i(x, y)$$



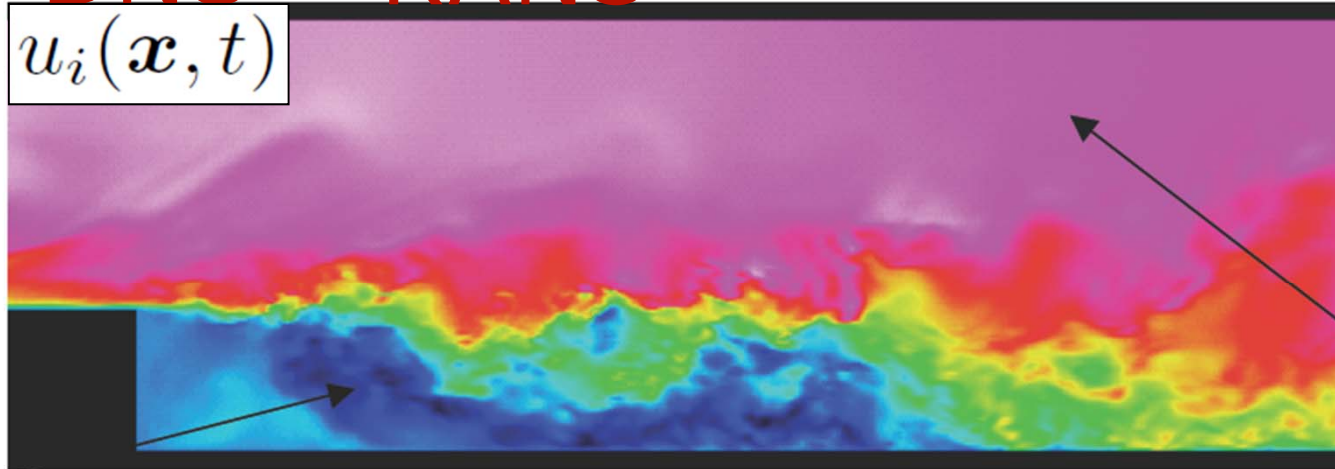
Length of the recirculation region is of engineering interest

# DNS – RANS

**DNS**

Istantaneous

$$u_i(\mathbf{x}, t)$$



low velocity regions

high velocity regions

DNS (and also LES):

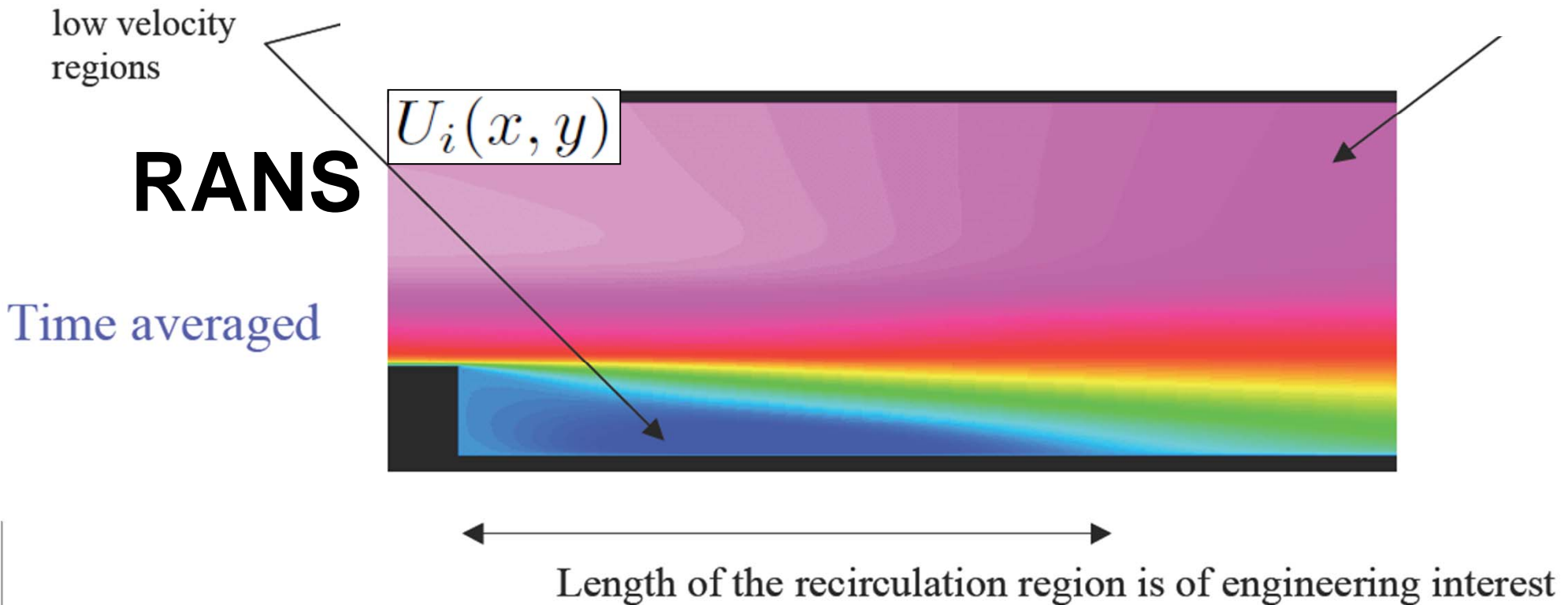
- 3D
- Time dependent
  - Full information of turbulence scales
  - Acoustics and dynamic loads
- Huge Reynolds number dependency

**Expensive!**

# DNS – RANS

RANS:

- Reduction of dimensions → cheap  
Here: 2D and steady
- Only statistical information of turbulence scales:  
Time and length scales  
rms values



# Scale separation



- Large scales  $L$  and  $U$  related to geometrical scales
- Small viscous scales (related to  $\nu$  and  $\varepsilon$ )

$$l_K = \eta \sim \left(\frac{\nu^3}{\varepsilon}\right)^{1/4}, \quad t_K \sim \sqrt{\frac{\nu}{\varepsilon}}$$

- Scale separation

$$\frac{L}{\eta} \sim Re^{3/4}, \quad \frac{t}{t_K} \sim Re^{1/2}$$

- Reynolds number

$$Re = \frac{LU}{\nu}$$

# Different Reynolds numbers



- Based on global scales

$$Re_L = \frac{LU}{\nu}$$

- Based on distance  $x$  from leading edge (flat plate)

$$Re_x = \frac{xU}{\nu}$$

- Based on boundary layer thickness ( $\delta$ )

$$Re_\delta = \frac{\delta U}{\nu}$$

- Based on wall skin friction

$$Re_\tau = \frac{\delta u_\tau}{\nu}$$

# Viscosity

- Kinematic viscosity,  $\nu$
- Dynamic viscosity,  $\mu$
- Density,  $\rho$

$$\mu = \rho\nu$$



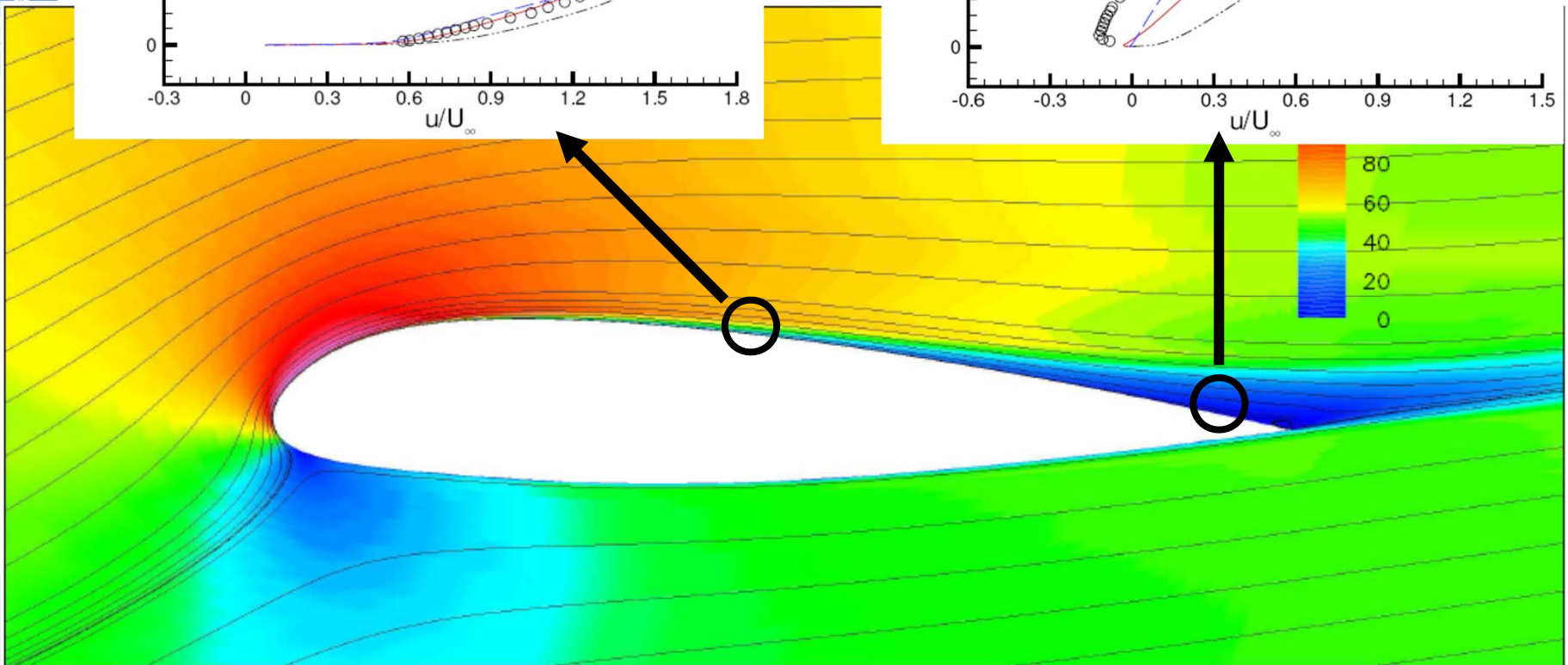
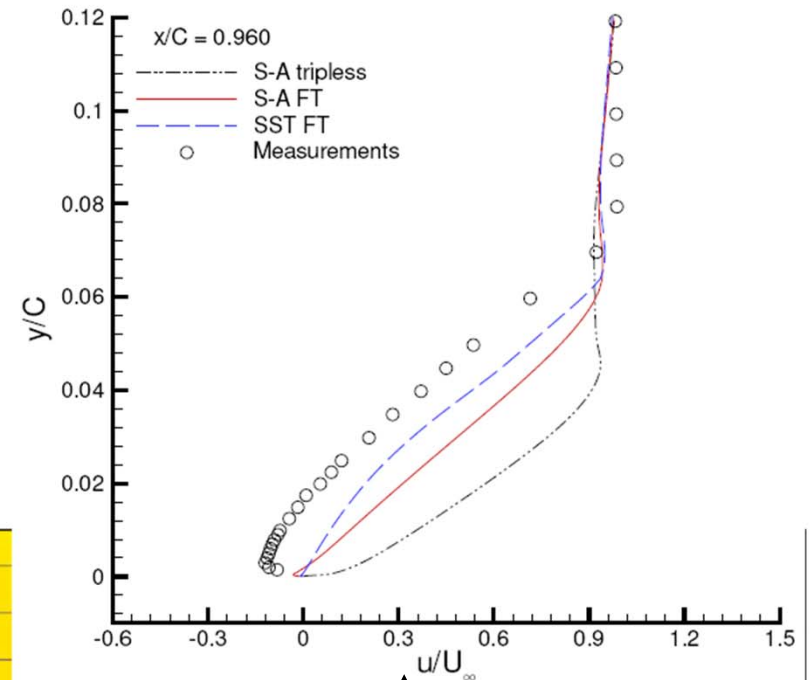
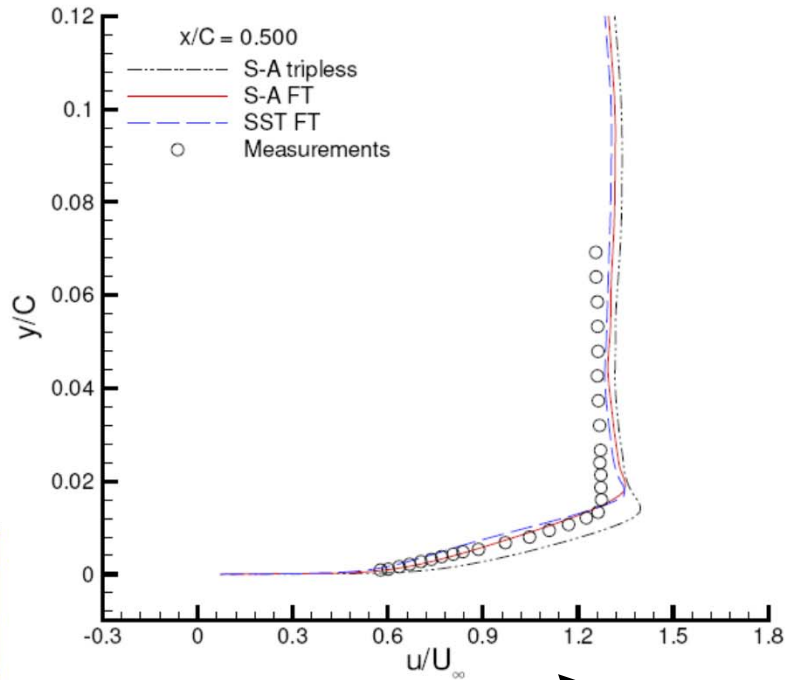


# Boundary layers (BL)



- Thin layers
  - Thickness Reynolds number dependent
- Laminar boundary layers
  - Thickness related to wall skin friction
- Turbulent boundary layers
  - Inner and outer scales separated
  - Scale separation Reynolds number dependent
  
- Figures (Wing+bl – bl – near-wall)

# BL on the ONERA A-profile



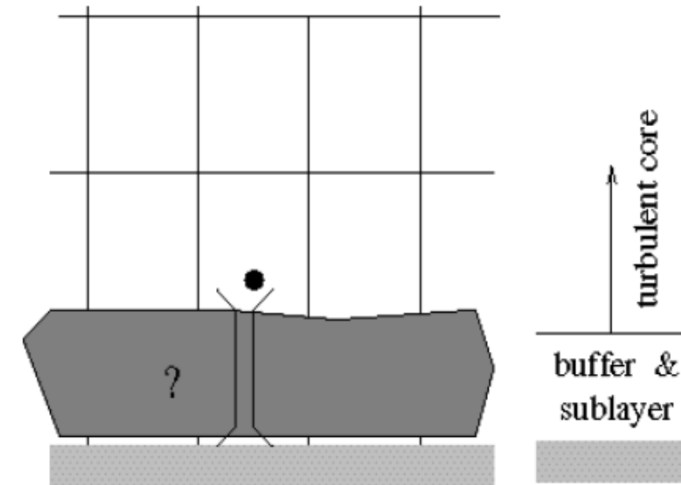
# Approximation of BLs



- Slip wall boundary condition
  - Boundary layer completely neglected
  - Euler (non-viscous) computations possible
  - Slip BC can also be applied to viscous & turbulent CFD
- No slip boundary condition
  - Boundary layer completely resolved ( $y^+ = 1$ )
  - Extreme resolution needed ( $\Delta y = 1-100\mu\text{m}$ )
  - 40-80 grid points within the boundary layer
- Log-law boundary condition (turbulence)
  - First grid point within log layer ( $y^+ > 20$  AND  $y < 0.1\delta$ )
  - 10-20 grid points within the boundary layer
  - Warning: standard log-law BCs inconsistent with too small grid size. READ SOLVER DOCUMENTATION !!!

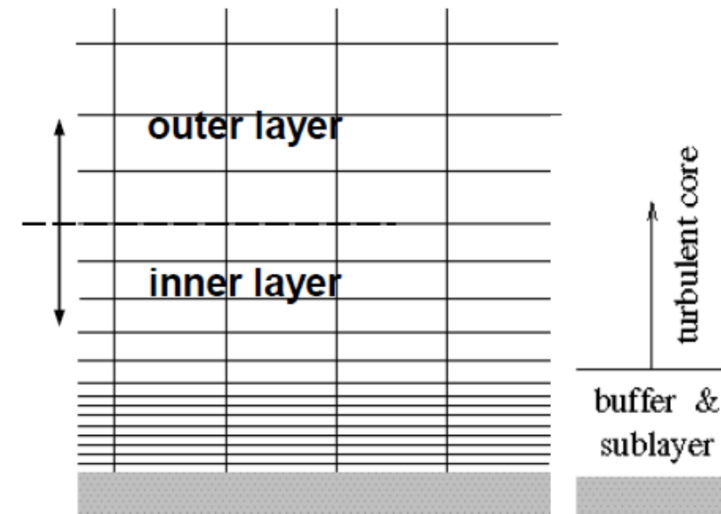
# What's in Fluent?

- Standard and Non-Equilibrium Wall Functions:
  - “Wall adjacent cells should have  $y^+$  values between 30 and 300–500” – (remember  $y < 0.1\delta!$  )
  - “The mesh expansion ratio should be small (no larger than around 1.2)”
  - “Non-equilibrium wall function method attempts to improve the results for flows with higher pressure gradients, separations, reattachment and stagnation”
- Scalable Wall Functions:
  - Consistent for all  $y^+$  values



# What's in Fluent? ...

- Enhanced Wall Treatment Option
  - Combines a blended law-of-the wall and a two-layer zonal model.
  - Suitable for low-Re flows or flows with complex near-wall phenomena.
  - Generally requires a fine near-wall mesh capable of resolving the viscous sublayer
  - $y^+ < 5$ , and a minimum of 10–15 cells across the “inner layer” for best results
  - Valid for all  $y^+$
  - Available for all k-e and k-w models
  - Not yet for Spalart-Allmaras ( $y^+ < 3$  OR  $y^+ > 15$ )



# Recommendations for Fluent

- For  $K-\varepsilon$  models
  - use Enhanced Wall Treatment: EWT- $\varepsilon$
- If wall functions are favored with  $K-\varepsilon$  models
  - use scalable wall functions
- For  $K-\omega$  models
  - use the default: EWT- $\omega$



# Wall bounded turbulence

- Viscous wall scales

$$l_* = \frac{\nu}{u_\tau}, \quad t_* = \frac{\nu}{u_\tau^2}$$

- Wall friction velocity

$$u_\tau = \sqrt{\frac{\tau_w}{\rho}} = \sqrt{\nu \left. \frac{\partial U}{\partial y} \right|_{\text{wall}}} = U \sqrt{\frac{1}{2} C_f}$$

- Friction coefficient

$$C_f = \frac{\tau_w}{\frac{1}{2} \rho U^2} = 2 \left( \frac{u_\tau}{U} \right)^2$$

- Viscous wall distance

$$y^+ = \frac{y}{l_*} = \frac{y u_\tau}{\nu}$$



# Empirical relations for BLs

- Friction coefficient

- Turbulent  $\frac{C_f}{2} \approx 0,0296 Re_x^{-1/5}$

- Laminar  $\frac{C_f}{2} = 0,332 Re_x^{-1/2}$

- Boundary layer thickness

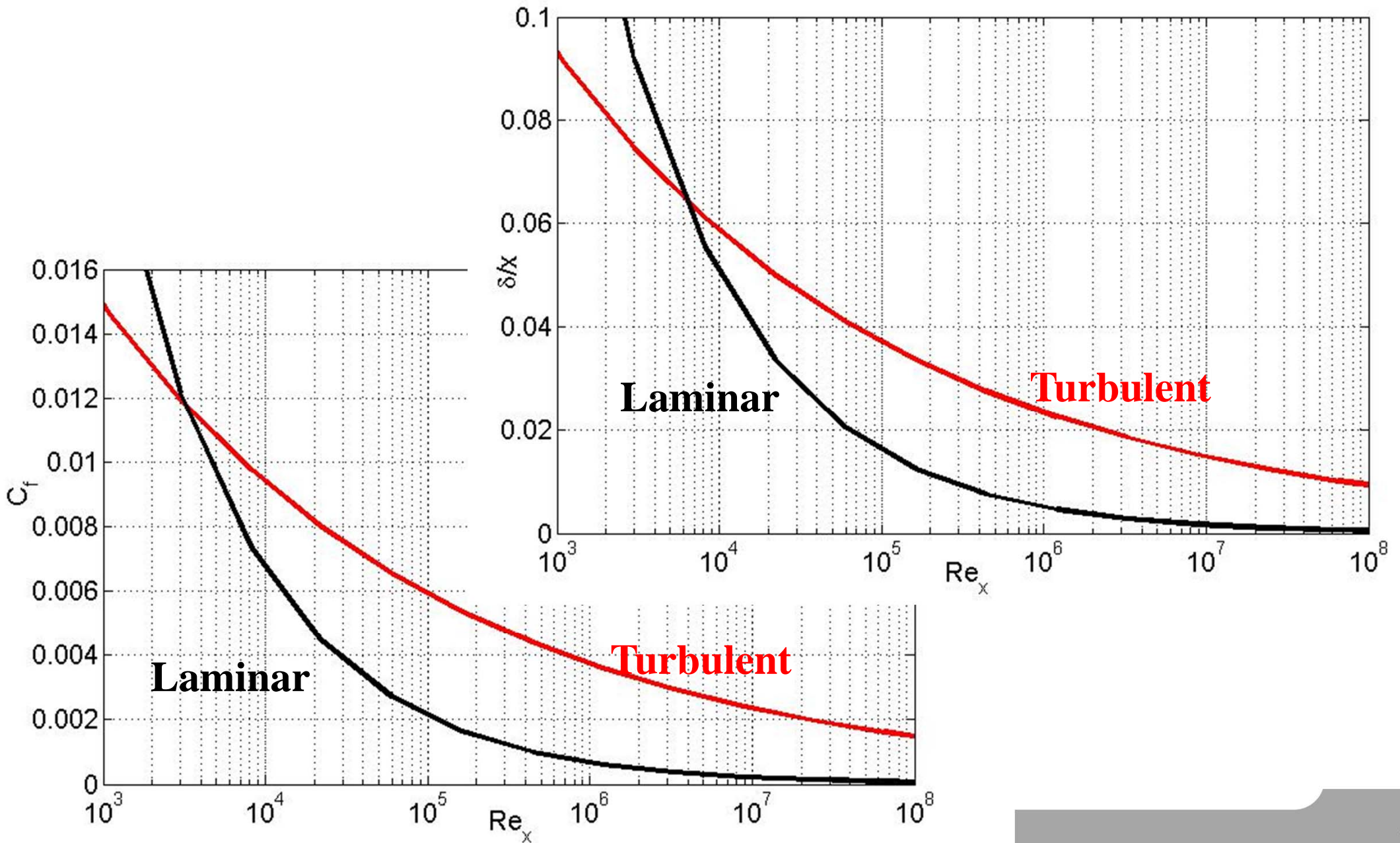
- Turbulent  $\frac{\delta}{x} \approx 0,37 Re_x^{-1/5}$

- Laminar  $\frac{\delta}{x} = 5,0 Re_x^{-1/2}$

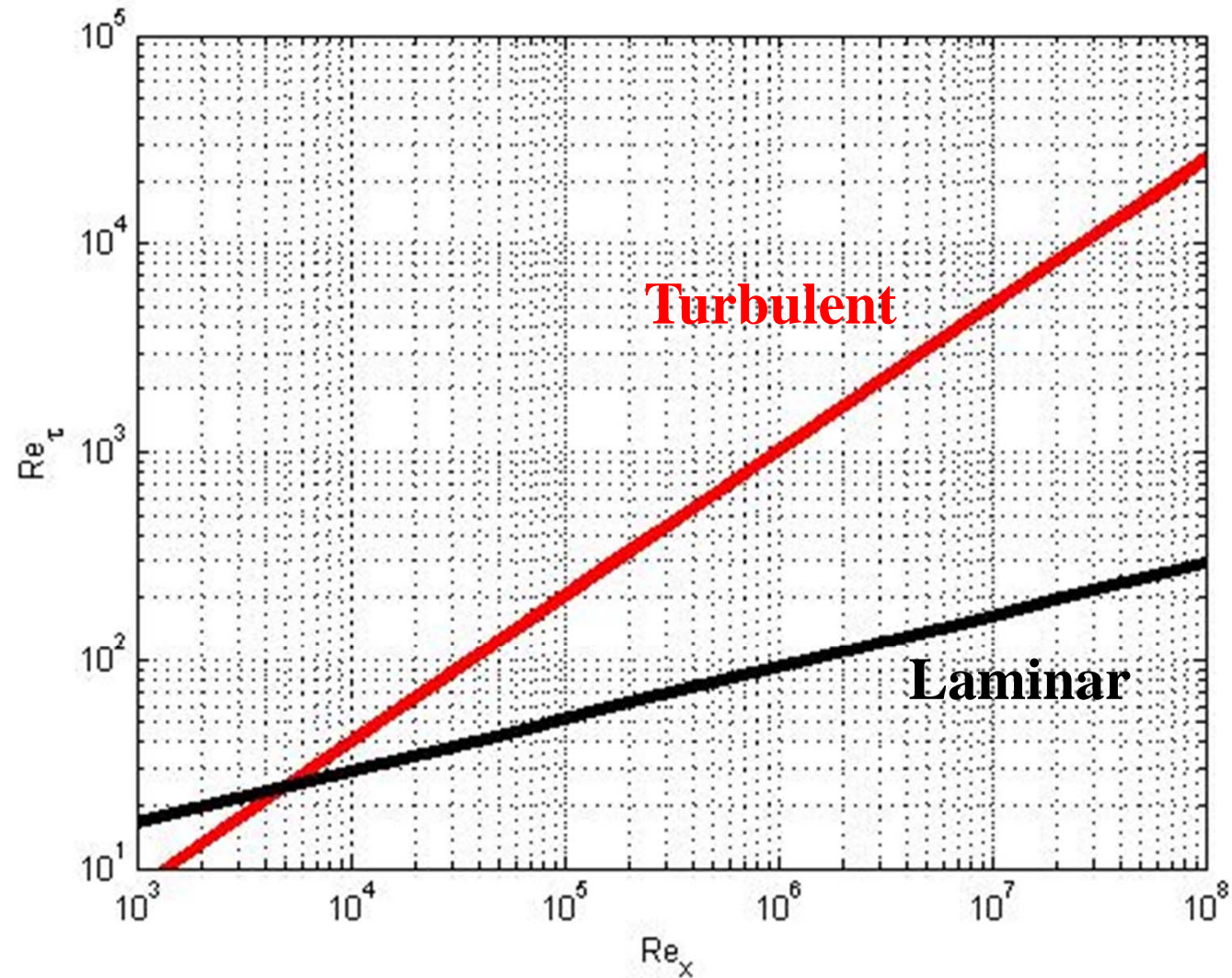




# Empirical relations plotted



# Empirical relations plotted



# Turbulence modelling

- Reynolds decomposition

$$\tilde{u}_i(\mathbf{x}, t) = U_i(\mathbf{x}) + u_i(\mathbf{x}, t)$$

$$\text{where } U_i(\mathbf{x}) = \overline{\tilde{u}_i(\mathbf{x}, t)} \text{ and } \overline{u_i(\mathbf{x}, t)} = 0$$

- The “mean” is time average, ensemble average or averaging in homogeneous directions.  $U_i(\mathbf{x})$  may actually vary in time with a time scale much longer than the turbulent time scale.
- Take the mean of the Navier-Stokes equations -> RANS

$$\frac{\partial U_i}{\partial x_i} = 0$$

$$\frac{\partial U_i}{\partial t} + U_k \frac{\partial U_i}{\partial x_k} = -\frac{1}{\rho} \frac{\partial P}{\partial x_i} + \frac{\partial}{\partial x_k} \left( \nu \frac{\partial U_i}{\partial x_k} - \overline{u_i u_k} \right)$$



# Reynolds stresses



- Not “small”
- Significant effects on the flow
- Needs to be modelled in terms of mean flow quantities
- Reduces the problem to steady (or slowly varying)
- 2D assumptions possible
  
- Equation can be derived from Navier-Stokes equations
- Need modelling

# Eddy-viscosity models (EVM)

- Assume: Reynolds stresses related to an “eddy viscosity”,  $\nu_T$

$$\overline{u_i u_j} = -2\nu_T S_{ij} \quad \left( + \frac{1}{3} \overline{u_k u_k} \delta_{ij} \right)$$

$$\text{where } S_{ij} = \frac{1}{2} \left( \frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right)$$

Based on Boussinesq (1877)

- Eddy viscosity  $\sim$  turbulence velocity  $V$  and length  $L$  scales:  $\nu_T \sim VL$



# One-equation models



- One transport equation for  $K$  (turbulent kinetic energy) or  $\nu_T$ .
- Additional information from global conditions (typically wall distance)
- Works well for attached boundary layers
- Not very general, but more than algebraic models
- Example: Spalart-Allmaras (1992)
  - reasonable and robust model for external aerodynamics
  - Boeing's "standard model"

# Two-equation models



- Two transport equations for the turbulence scales ( $K-\varepsilon$  or  $K-\omega$ )
- Completely determined in terms of local quantities (except near-wall corrections which may be dependent on wall distance)
- Works well for attached boundary layers
- Somewhat more general than zero-, one-equation models
- Model transport equations loosely connected to the exact equations.
  
- Examples:
  - Standard  $K-\varepsilon$  model (Launder & Spalding 1974)
  - Wilcox  $K-\omega$  (1988, ...) models
  - Menter (1994) SST  $K-\omega$  model (performing reasonable well also in separated flows)
    - Airbus' "standard model"

# Eddy-viscosity models ...



- Problems:
  - No dependency on rotation or curvature. Real turbulence strongly dependent.
  - Modelled production proportional to strain rate squared  $\sim S^2$ . Exact production  $\sim S$ . Results in a overestimated production of  $K$  in highly sheared flows (around stagnation points, impinging jets, pressure gradient BLs, separated flows).
- Fixes
  - Rotation & curvature corrections
  - Yap correction (limit excessive turbulent lengthscale)
  - Menter SST correction (limit excessive  $v_T$ ).



# LES and LES/RANS hybrids



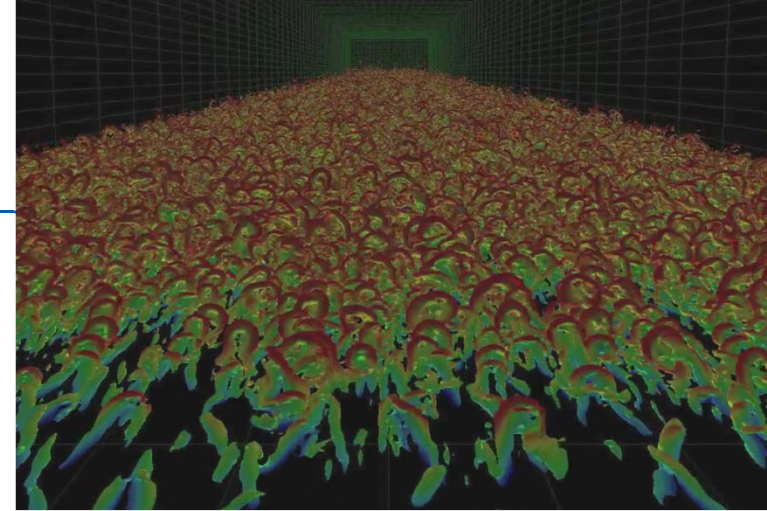
- Simulation of only the large scale turbulence (compare with DNS, simulation of all scales)
  - Always time dependent and 3D -> expensive
- Wall free turbulence simulations almost  $Re$  independent
- Wall bounded turbulence largely  $Re$  dependent
  - fully resolved near-wall region very expensive (almost as DNS)
  - wall-function or near-wall RANS coupling saves computational cost
  - hybrid RANS-LES (RANS in attached BLs and LES in wall-free separated regions) a very active research field, eg DES

# LES and LES/RANS hybrids ...



- LES in academic research for:
  - low  $Re$  generic flows
  - complement to DNS for higher  $Re$
  - gives detailed knowledge about turbulence
- LES in industrial use in:
  - internal flow with complex geometries
  - flows around blunt bodies (with large separated regions)
  - atmospheric boundary layers (e.g. weather forecasts)
  - combustion simulation
  - other complex flow physics at moderate  $Re$
- Warning: LES is extremely expensive in high attached and slightly separated wall-bounded flows, if properly resolved.

# How expensive is DNS?



- **DNS of flat plate turbulent boundary layer**
  - Schlatter, et al., KTH, Dept. of Mechanics
  - APS meeting 2010: <http://arxiv.org/abs/1010.4000>
  - <http://www.youtube.com/watch?v=4KeaAhVoPIw>
  - <http://www.youtube.com/watch?v=zm9-hSP4s3w>
  - $Re_\theta = 4300$
  - $8192 \times 513 \times 768 = 3.2 \times 10^9$  spectral modes ( $7.5 \times 10^9$  nodes)
  - $\Delta x^+ = 9, \Delta z^+ = 4 \rightarrow$  box:  $L^+ = 70\,000, H^+ = W^+ = 3\,000$
  - BL relations:  $Re_x = 1.4 \times 10^6$
  - CPU time: 3 months @ 4000 CPU cores = 1 unit
- **DNS of model airplane, same Reynolds number ( $Re_x = 1.4 \times 10^6$ )**
  - Only a narrow stripe – wing requires about 1 000 stripes
  - $N_{\text{nodes}} = 10^{13}$
  - CPU =  $10^3$  units

# Empirical turbulent BL relations

- **Skin friction coefficient:**  $\frac{C_f}{2} = \frac{\tau_w}{\rho U_\infty^2} = \left( \frac{Re_\tau}{Re_\delta} \right)^2 \approx 0.0296 Re_x^{-1/5}$
- **Boundary layer thickness:**  $\frac{\delta}{x} = \frac{Re_\delta}{Re_x} \approx 0.37 Re_x^{-1/5}$
- **Boundary layer momentum thickness:**  $Re_\tau \approx 1.13 Re_\theta^{0.843}$
- **Reynolds numbers:**  
 $Re_\tau \equiv \frac{\delta u_\tau}{\nu}$      $Re_\theta \equiv \frac{\theta U_\infty}{\nu}$      $Re_\delta \equiv \frac{\delta U_\infty}{\nu}$      $Re_x \equiv \frac{x U_\infty}{\nu}$

# DNS – full scale airplane

- Re scaling – wall bounded flow

- **Nodes:**  $N_{nodes} \sim \frac{L \times B \times H}{\Delta x \Delta z \Delta y} \sim L^{+2} H^{+} \sim Re_x^{5/2}$

- **Time steps:**  $N_{\Delta T} \sim \frac{T}{\Delta T} \sim T^{+} \sim Re_x^{4/5}$

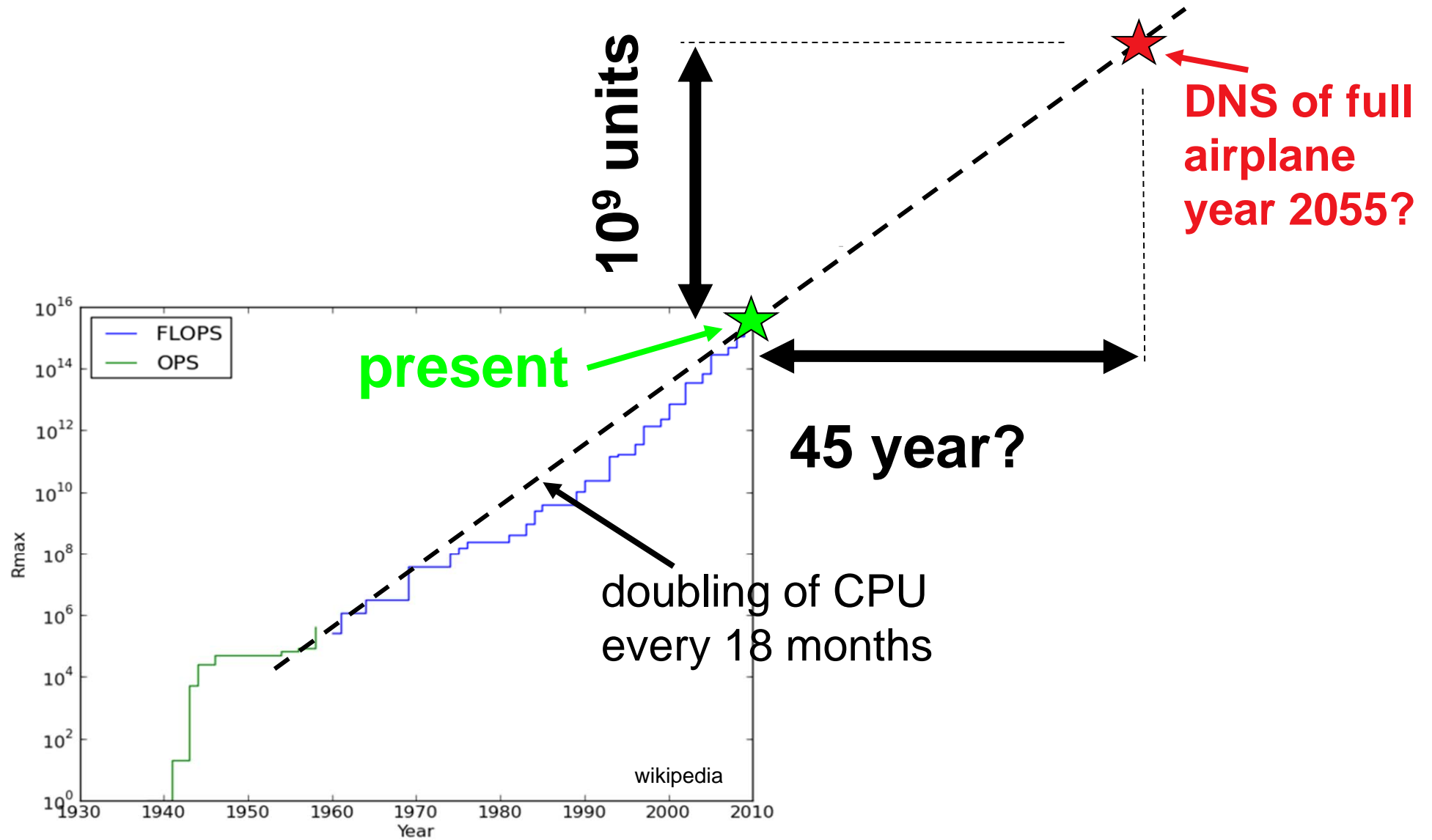
- **CPU time:**  $N_{CPU} \sim N_{nodes} \times N_{\Delta T} \sim Re_x^{33/10}$

- DNS of Airplane ( $Re_x = 70 \times 10^6$ ) (factor of 50)

- **$N_{nodes} = 10^{17}$**

- **CPU =  $10^9$  units**

# Supercomputer development



# Computational effort – different approaches

Name	Aim	Unsteady	<i>Re</i> -dependence	3/2D	Empiricism	Grid	Steps	Ready
2DURANS	Numerical	Yes	Weak	No	Strong	$10^5$	$10^{3.5}$	1980
3DRANS	Numerical	No	Weak	No	Strong	$10^7$	$10^3$	1990
3DURANS	Numerical	Yes	Weak	No	Strong	$10^7$	$10^{3.5}$	1995
DES	Hybrid	Yes	Weak	Yes	Strong	$10^8$	$10^4$	2000
LES	Hybrid	Yes	Weak	Yes	Weak	$10^{11.5}$	$10^{6.7}$	2045
QDNS	Physical	Yes	Strong	Yes	Weak	$10^{15}$	$10^{7.3}$	2070
DNS	Numerical	Yes	Strong	Yes	None	$10^{16}$	$10^{7.7}$	2080

From Spalart, Int. J. Heat and Fluid Flow, 2000

- **RANS: Reynolds Averaged Navier-Stokes**
- **URANS: Unsteady RANS – slowly in time**
- **DES: Detached Eddy Simulation**
- **LES: Large eddy simulation**
- **QDNS: Quasi DNS, or wall resolved LES**
- **DNS: Direct Numerical Simulation (of the Navier-Stokes eq's)**
- **“Ready”**: When first results can be expected